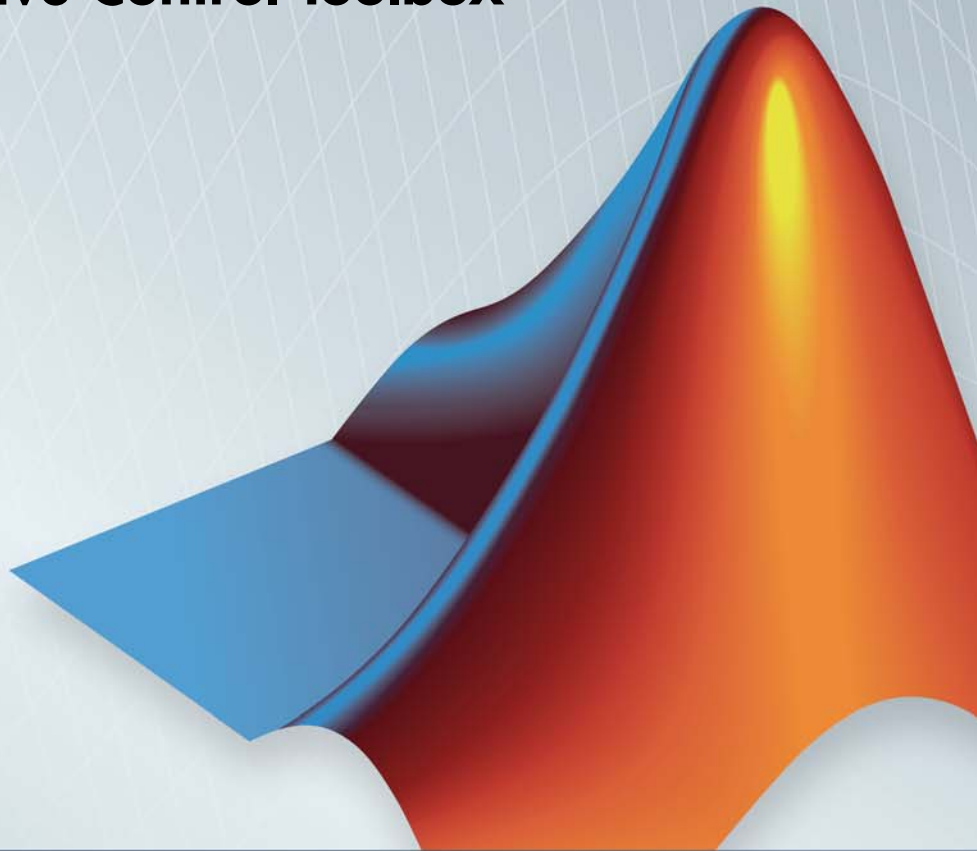


# Model Predictive Control Toolbox™

## Reference

**R2014a**

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March 2014	Online only	Revised for Version 4.2 (Release R2014a)



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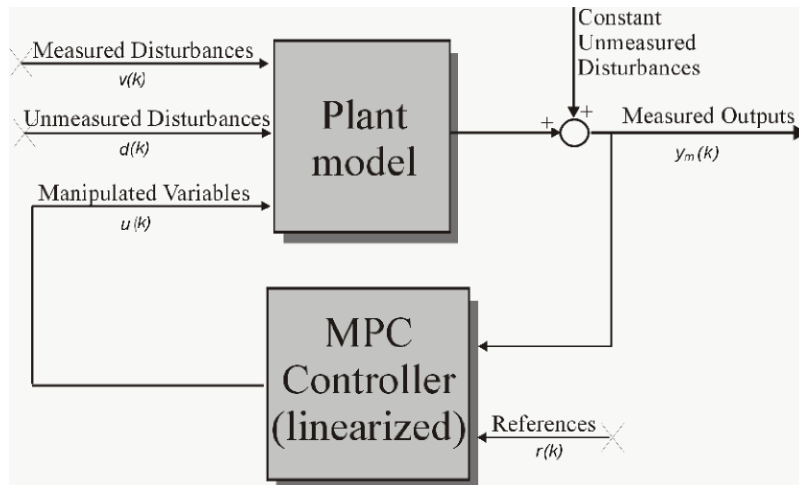
---

# clffset

**Purpose** Compute MPC closed-loop DC gain from output disturbances to measured outputs assuming constraints are inactive at steady state

**Syntax** `DCgain=clffset(MPCobj)`

**Description** The `clffset` function computes the DC gain from output disturbances to measured outputs, assuming constraints are not active, based on the feedback connection between `Model.Plant` and the linearized MPC controller, as depicted below.



## Computing the Effect of Output Disturbances

By superposition of effects, the gain is computed by zeroing references, measured disturbances, and unmeasured input disturbances.

`DCgain=clffset(MPCobj)` returns an  $n_{ym}$ -by- $n_{ym}$  DC gain matrix `DCgain`, where  $n_{ym}$  is the number of measured plant outputs. `MPCobj` is the MPC object specifying the controller for which the closed-loop gain is calculated. `DCgain(i, j)` represents the gain from an additive (constant) disturbance on output  $j$  to measured output  $i$ . If row  $i$  contains all zeros, there will be no steady-state offset on output  $i$ .



**See Also**

mpc | ss

**Related  
Examples**

- “Compute Steady-State Gain”

# compare

---

**Purpose** Compare two MPC objects

**Syntax** `yesno=compare(MPC1,MPC2)`

**Description** The compare function compares the contents of two MPC objects MPC1, MPC2. If the design specifications (models, weights, horizons, etc.) are identical, then `yesno` is equal to 1.

---

**Note** compare may return `yesno=1` even if the two objects are not identical. For instance, MPC1 may have been initialized while MPC2 may have not, so that they may have different sizes in memory. In any case, if `yesno=1` the behavior of the two controllers will be identical.

---

**See Also** `mpc` | `pack`

**Purpose** Change MPC controller's sampling time

**Syntax** `MPCobj=d2d(MPCobj,ts)`

**Description** The `d2d` function changes the sampling time of the MPC controller `MPCobj` to `ts`. All models are sampled or resampled as soon as the QP matrices must be computed, e.g., when `sim` or `mpcmove` are used.

**See Also** `mpc` | `set`

# get

---

## Purpose

MPC property values

## Syntax

```
Value = get(MPCObj, 'PropertyName')  
Struct = get(MPCObj)  
get(MPCObj)
```

## Description

`Value = get(MPCObj, 'PropertyName')` returns the current value of the property `PropertyName` of the MPC controller `MPCObj`. The string `'PropertyName'` can be the full property name (for example, `'UserData'`) or any unambiguous case-insensitive abbreviation (for example, `'user'`). You can specify any generic MPC property.

`Struct = get(MPCObj)` converts the MPC controller `MPCObj` into a standard MATLAB<sup>®</sup> structure with the property names as field names and the property values as field values.

`get(MPCObj)` without a left-side argument displays all properties of `MPCObj` and their values.

## Tips

An alternative to the syntax

```
Value = get(MPCObj, 'PropertyName')
```

is the structure-like referencing

```
Value = MPCObj.PropertyName
```

For example,

```
MPCObj.Ts  
MPCObj.p
```

return the values of the sampling time and prediction horizon of the MPC controller `MPCObj`.

## See Also

[mpc](#) | [set](#)

**Purpose** Model Predictive Control custom constraint definitions

**Syntax** [E,F,G,V,S] = getconstraint(mpcobj)

**Description** [E,F,G,V,S] = getconstraint(mpcobj) returns the custom constraints previously defined for the mpc object, mpcobj. The constraints are in the general form

$$Eu(k+j) + Fy(k+j) + Sv(k+j) \leq G + \varepsilon V \quad (1-1)$$

where:

- $p$  — MPC prediction horizon.
- $k$  — current time index.
- $u$  — column vector of manipulated variables.
- $y$  — column vector of all plant output variables.
- $v$  — column vector of measured disturbance variables.
- $\varepsilon$  — scalar slack variable used for constraint softening.
- $E, F, G, V$  and  $S$  — constant matrices.

getconstraint calculates the last constraint at time  $k+p$  assuming that  $u(k+p|k) = u(k+p-1|k)$ . This is because  $u(k+p|k)$  is not optimized by the model predictive controller.

**Input Arguments** **mpcobj**  
MPC controller, specified as an mpc object.

**Output Arguments** **E**  
Constant used in custom constraints as defined in Equation 1-1.

[ ] if mpcobj contains no custom constraints.

E is an  $n_c$ -by- $n_u$  matrix, where  $n_c$  is the number of custom constraints and  $n_u$  is the number of manipulated variables.

## **F**

Constant used in custom constraints as defined in Equation 1-1.

[ ] if `mpcobj` contains no custom constraints.

**F** is an  $n_c$ -by- $n_y$  matrix, where  $n_c$  is the number of custom constraints and  $n_y$  is the number of output variables (measured and unmeasured).

## **G**

Constant used in custom constraints as defined in Equation 1-1.

[ ] if `mpcobj` contains no custom constraints.

**G** is an  $n_c$ -by-1 vector, where  $n_c$  is the number of custom constraints.

## **V**

Constant used in custom constraints as defined in Equation 1-1.

[ ] if `mpcobj` contains no custom constraints.

**V** is an  $n_c$ -by-1 vector, where  $n_c$  is the number of custom constraints.

If

- $V(i) = 0$  — the  $i^{\text{th}}$  constraint is hard
- $V(i) > 0$  — the  $i^{\text{th}}$  constraint is soft

Where  $i = 1, \dots, n_c$ .

In general, as  $V(i)$  decreases, the controller decreases the allowed constraint violation, i.e. the constraint becomes harder.

## **S**

Constant used in custom constraints as defined in Equation 1-1.

[ ] if `mpcobj` contains no custom constraints or there are no measured disturbances in the custom constraints.

**S** is an  $n_c$ -by- $n_{md}$  matrix, where  $n_c$  is the number of custom constraints and  $n_{md}$  is the number of measured disturbance inputs.

**Examples**

Obtain the constraints associated with an MPC controller.

Create an mpc object with 2 manipulated variables and 2 measured outputs.

```
p = rss(3,2,3);
p.D = 0;
p = setmpcsignals(p,'mv',[1 2],'md',3);
c = mpc(p,0.1);
```

Assume that you have two soft constraints.

$$u_1 + u_2 \leq 5$$

$$y_2 + v \leq 10$$

Set the constraints for the mpc object.

```
E = [1 1; 0 0];
F = [0 0; 0 1];
G = [5;10];
V = [1;1];
S = [0;1];
setconstraint(c,E,F,G,V,S);
```

Obtain the constraints for c.

```
[E F G V S] = getconstraint(c)
E =
```

```
    1    1
    0    0
```

```
F =
```

```
    0    0
    0    1
```

# getconstraint

---

G =

5  
10

V =

1  
1

S =

0  
1

## See Also

`setconstraint`



**Purpose**

Model and gain for observer design

**Syntax**

```
M = getestim(MPCobj)
[M,A,Cm] = getestim(MPCobj)
[M,A,Cm,Bu,Bv,Dvm] = getestim(MPCobj)
[M,model,Index] = getestim(MPCobj,'sys')
```

**Description**

M = getestim(MPCobj) extracts the estimator gain M used by the MPC controller MPCobj for observer design. The observer is based on the models specified in MPCobj.Model.Plant, in MPCobj.Model.Disturbance, by the output disturbance model (default is integrated white noise, see “Output Disturbance Model”), and by MPCobj.Model.Noise.

The state estimator is based on the linear model (see “State Estimation”)

$$x(k + 1) = Ax(k) + B_u u(k) + B_v v(k)$$

$$y_m(k) = C_m x(k) + D_{vm} v(k)$$

where  $v(k)$  are the measured disturbances,  $u(k)$  are the manipulated plant inputs,  $y_m(k)$  are the measured plant outputs, and  $x(k)$  is the overall state vector collecting states of plant, unmeasured disturbance, and measurement noise models.

The estimator used in the Model Predictive Control Toolbox™ software is described in “State Estimation”. The estimator’s equations are

**Predicted Output Computation:**

$$\hat{y}_m(k|k-1) = C_m \hat{x}(k|k-1) + D_{vm} v(k)$$

**Measurement Update:**

$$\hat{x}(k|k) = \hat{x}(k|k-1) + M(y_m(k) - \hat{y}_m(k|k-1))$$

**Time Update:**

$$\hat{x}(k+1|k) = A\hat{x}(k|k) + B_u u(k) + B_v v(k)$$

By combining these three equations, the overall state observer is

$$\hat{x}(k+1|k) = (A - LC_m)\hat{x}(k|k-1) + Ly_m(k) + B_u u(k) + (B_v - LD_{vm})v(k)$$

where  $L=AM$ .

`[M,A,Cm] = getestim(MPCobj)` also returns matrices  $A, C_m$  used for observer design. This includes the plant model, disturbance model, noise model, and offsets. The extended state is

$$x = [\text{plant states}; \text{disturbance models states}; \text{noise model states}]$$

`[M,A,Cm,Bu,Bv,Dvm] = getestim(MPCobj)` retrieves the whole linear system used for observer design.

`[M,model,Index] = getestim(MPCobj, 'sys')` retrieves the overall model used for observer design (specified in the `Model` field of the MPC object) as an LTI state-space object, and optionally a structure `Index` summarizing I/O signal types.

The extended input vector of model `model` is

$$u = [\text{manipulated vars}; \text{measured disturbances}; 1; \text{noise exciting disturbance model}; \text{noise exciting noise model}]$$

Model `model` has an extra measured disturbance input `v=1` used for handling possible nonequilibrium nominal values (see “Offsets”).

Input, output, and state names and input/output groups are defined for model `model`.

The structure `Index` has the fields detailed in the following table.

Field Name	Description
ManipulatedVariables	Indices of manipulated variables within input vector
MeasuredDisturbances	Indices of measured disturbances within input vector (not including offset=1)

Field Name	Description
Offset	Index of offset=1
WhiteNoise	Indices of white noise signals within input vector
MeasuredOutputs	Indices of measured outputs within output vector
UnmeasuredOutputs	Indices of unmeasured outputs within output vector

To improve the solvability of the Kalman filter design, the software adds white noise to the manipulated variables and measured disturbances, as described in “State Observer”. The model returned by `getestim` does not include this additional white noise.

**See Also**`setestim | mpc | mpcstate`

# getindist

---

**Purpose** Unmeasured input disturbance model

**Syntax** `model=getindist(MPCobj)`

**Description** `model=getindist(MPCobj)` retrieves the linear discrete-time transfer function used to model unmeasured input disturbances in the MPC setup described by the MPC object `MPCobj`. Model `model` is an LTI object with as many outputs as the number of unmeasured input disturbances, and as many inputs as the number of white noise signals driving the input disturbance model.

For details about the overall model used in the MPC algorithm for state estimation purposes, see “State Estimation”.

**See Also** `mpc` | `setindist` | `setestim` | `getestim` | `getoutdist`

**Purpose** Private MPC data structure

---

**Note** getmpcdata will be removed in a future version. Use get, getconstraint, getestim, getindist and getoutdist instead.

---

**Syntax** mpcdata=getmpcdata(MPCobj)

**Description** mpcdata=getmpcdata(MPCobj) returns the private field MPCData of the MPC object MPCobj. Here, all internal QP matrices, models, estimator gains are stored at initialization of the object. You can manually change the private data structure using the setmpcdata command, although you may only need this for very advanced use of Model Predictive Control Toolbox software.

---

**Note** Changes to the data structure may easily lead to unpredictable results.

---

**See Also** setmpcdata | set | get

# getname

---

**Purpose** I/O signal names in MPC prediction model

**Syntax**  
`name=getname(MPCobj, 'input', I)`  
`name=getname(MPCobj, 'output', I)`

**Description**  
`name=getname(MPCobj, 'input', I)` returns the name of the I-th input signal in variable name. This is equivalent to `name=MPCobj.Model.Plant.InputName{I}`. The name property is equal to the contents of the corresponding Name field of `MPCobj.DisturbanceVariables` or `MPCobj.ManipulatedVariables`.  
`name=getname(MPCobj, 'output', I)` returns the name of the I-th output signal in variable name. This is equivalent to `name=MPCobj.Model.Plant.OutputName{I}`. The name property is equal to the contents of the corresponding Name field of `MPCobj.OutputVariables`.

**See Also** `setname` | `mpc` | `set`

**Purpose** Unmeasured output disturbance model

**Syntax** `outdist=getoutdist(MPCobj)`  
`[outdist,channels]=getoutdist(MPCobj)`

**Description** `outdist=getoutdist(MPCobj)` retrieves the linear discrete-time transfer function used to model output disturbances in the MPC setup described by the MPC object `MPCobj`. Model `outdist` is an LTI object with as many outputs as the number of measured + unmeasured outputs, and as many inputs as the number of white noise signals driving the output disturbance model.

For details about the overall model used in the MPC algorithm for state estimation purposes, see “State Estimation”.

`[outdist,channels]=getoutdist(MPCobj)` also returns the output channels where integrated white noise was added as an output disturbance model. This is only meaningful when the default output disturbance model is used, namely when `MPCobj.OutputVariables(i).Integrators` is empty for all channels `i`. The array `channels` is empty for output disturbance models.

**See Also** `mpc` | `setoutdist` | `setestim` | `getestim` | `getindist`

# gpc2mpc

---

**Purpose** Generate MPC controller using generalized predictive controller (GPC) settings

**Syntax**

```
mpc = gpc2mpc(plant)  
gpcOptions = gpc2mpc  
mpc = gpc2mpc(plant,gpcOptions)
```

**Description** *mpc* = gpc2mpc(*plant*) generates a single-input single-output MPC controller with default GPC settings and sampling time of the plant, *plant*. The GPC is a nonminimal state-space representation described in [1]. *plant* is a discrete-time LTI model with sampling time greater than 0.

*gpcOptions* = gpc2mpc creates a structure *gpcOptions* containing default values of GPC settings.

*mpc* = gpc2mpc(*plant*,*gpcOptions*) generates an MPC controller using the GPC settings in *gpcOptions*.

- Tips**
- For plants with multiple inputs, only one input is the manipulated variable, and the remaining inputs are measured disturbances in feedforward compensation. The plant output is the measured output of the MPC controller.
  - Use the MPC controller with Model Predictive Control Toolbox software for simulation and analysis of the closed-loop performance.

**Input Arguments**

**plant**  
Discrete-time LTI model with sampling time greater than 0.

**gpcOptions**  
GPC settings, specified as a structure with the following fields.



N1	Starting interval in prediction horizon, specified as a positive integer. <b>Default:</b> 1.
N2	Last interval in prediction horizon, specified as a positive integer greater than N1. <b>Default:</b> 10.
NU	Control horizon, specified as a positive integer less than the prediction horizon. <b>Default:</b> 1.
Lam	Penalty weight on changes in manipulated variable, specified as a positive integer greater than or equal to 0. <b>Default:</b> 0.
T	Numerator of the GPC disturbance model, specified as a row vector of polynomial coefficients whose roots lie within the unit circle. <b>Default:</b> [1].
MVindex	Index of the manipulated variable for multi-input plants, specified as a positive integer. <b>Default:</b> 1.

## Examples

Design an MPC controller using GPC settings:

```
% Specify the plant described in Example 1.8 of [1].
G = tf(9.8*[1 -0.5 6.3],conv([1 0.6565],[1 -0.2366 0.1493]));

% Discretize the plant with sample time of 0.6 seconds.
Ts = 0.6;
Gd = c2d(G, Ts);

% Create a GPC settings structure.
```

```
GPCOptions = gpc2mpc;

% Specify the GPC settings described in example 4.11 of [1].
% Hu
GPCOptions.NU = 2;
% Hp
GPCOptions.N2 = 5;
% R
GPCOptions.Lam = 0;
GPCOptions.T = [1 -0.8];

% Convert GPC to an MPC controller.
mpc = gpc2mpc(Gd, GPCOptions);

% Simulate for 50 steps with unmeasured disturbance between
% steps 26 and 28, and reference signal of 0.
SimOptions = mpcsimopt(mpc);
SimOptions.UnmeasuredDisturbance = [zeros(25,1); ...
-0.1*ones(3,1); 0];
sim(mpc, 50, 0, SimOptions);
```

## References

[1] Maciejowski, J. M. *Predictive Control with Constraints*, Pearson Education Ltd., 2002, pp. 133–142.

## See Also

- “MPC Controller Object” on page 3-2
- “Design Controller Using the Design Tool”
  - “Design Controller at the Command Line”

**Purpose**

Create MPC controller

**Syntax**

```
MPCobj=mpc(plant)
MPCobj=mpc(plant,ts)
MPCobj=mpc(plant,ts,p)
MPCobj=mpc(plant,ts,p,m)
MPCobj=mpc(plant,ts,p,m,W)
MPCobj=mpc(plant,ts,p,m,W,MV,OV,DV)
MPCobj=mpc(models,ts,p,m,W,MV,OV,DV)
```

**Description**

`MPCobj=mpc(plant)` creates an MPC controller based on the discrete-time model `plant`. The model can be specified either as an LTI object, or as an object in System Identification Toolbox™ format. See “Identify Plant from Data”.

`MPCobj=mpc(plant,ts)` specifies the sampling time `ts` for the MPC controller. A continuous-time `plant` is discretized with sampling time `ts`. A discrete-time `plant` is resampled if its sampling time is different than the controller’s sampling time `ts`. If `plant` is a discrete-time model with unspecified sampling time, namely `plant.ts=-1`, then Model Predictive Control Toolbox software assumes that the plant is sampled with the controller’s sampling time `ts`. `ts` has the same unit as the internal predictive plant model, i.e., `plant.TimeUnit`.

`MPCobj=mpc(plant,ts,p)` specifies the prediction horizon `p`.

`MPCobj=mpc(plant,ts,p,m)` specifies the control horizon `m`.

`MPCobj=mpc(plant,ts,p,m,W)` also specifies the structure `W` of input, input increments, and output weights (see “Weights” on page 3-7).

`MPCobj=mpc(plant,ts,p,m,W,MV,OV,DV)` also specifies limits on manipulated variables (`MV`) and output variables (`OV`), as well as equal concern relaxation values, units, etc. Names and units of input disturbances can be also specified in the optional input `DV`. The fields of structures `MV`, `OV`, and `DV` are described in “ManipulatedVariables” on page 3-3, in “OutputVariables” on page 3-4, and in “DisturbanceVariables” on page 3-6, respectively).

`MPCobj=mpc(model,ts,p,m,W,MV,OV,DV)` where `model` is a structure containing models for plant, unmeasured disturbances, measured disturbances, and nominal linearization values, as described in “Model” on page 3-9.

---

**Note** Other MPC properties are specified by using `set(MPCobj,Property1, Value1,Property2,Value2,...)` or `MPCobj.Property=Value`.

---

## Construction and Initialization

An MPC controller is built in two steps. The first step happens *at construction* when the object constructor `mpc` is invoked, or properties are changed by a `set` command. At this first stage, only basic consistency checks are performed, such as dimensions of signals, weights, constraints, etc. The second step happens *at initialization*, namely when the object is used for the first time by methods such as `mpcmove` and `sim`, that require the full computation of the QP matrices and the estimator gain. At this second stage, further checks are performed, such as a test of observability of the overall extended model.

Informative messages are displayed in the command window in both phases, you can turn them on or off using the `mpcverbosity` command.

## Properties

All the parameters defining the MPC control law (prediction horizon, weights, constraints, etc.) are stored in an MPC object, whose properties are listed in the following table (MPC Controller Object on page 3-2 ).

### MPC Controller Object

Property	Description
ManipulatedVariables (or MV or Manipulated or Input )	Input and input-rate upper and lower bounds, ECR values, names, units, and input target
OutputVariables (or OV or Controlled or Output )	Output upper and lower bounds, ECR values, names, units

### MPC Controller Object (Continued)

Property	Description
DisturbanceVariables (or DV or Disturbance )	Disturbance names and units
Weights	Weights defining the performance function
Model	Plant, input disturbance, and output noise models, and nominal conditions.
Ts	Controller's sampling time
Optimizer	Parameters for the QP solver
PredictionHorizon	Prediction horizon
ControlHorizon	Number of free control moves or vector of blocking moves
History	Creation time
Notes	Text or comments about the MPC controller object
UserData	Any additional data
MPCData (private)	Matrices for the QP problem and other accessorial data
Version (private)	Model Predictive Control Toolbox version number

### ManipulatedVariables

ManipulatedVariables (or MV or Manipulated or Input) is an  $n_u$ -dimensional array of structures ( $n_u$  = number of manipulated variables), one per manipulated variable. Each structure has the fields described in the following table (Structure ManipulatedVariables on page 3-3), where  $p$  denotes the prediction horizon.

**Structure ManipulatedVariables**

Field Name	Content	Default
Min	1 to $p$ dimensional vector of lower constraints on a manipulated variable $u$	-Inf
Max	1 to $p$ dimensional vector of upper constraints on a manipulated variable $u$	Inf
MinECR	1 to $p$ dimensional vector describing the equal concern for the relaxation of the lower constraints on $u$	0
MaxECR	1 to $p$ dimensional vector describing the equal concern for the relaxation of the upper constraints on $u$	0
Target	1 to $p$ dimensional vector of target values for the input variable $u$	'nominal'
RateMin	1 to $p$ dimensional vector of lower constraints on the rate of a manipulated variable $u$	-Inf if problem is unconstrained, otherwise -10
RateMax	1 to $p$ dimensional vector of upper constraints on the rate of a manipulated variable $u$	Inf
RateMinECR	1 to $p$ dimensional vector describing the equal concern for the relaxation of the lower constraints on the rate of $u$	0

**Structure ManipulatedVariables (Continued)**

Field Name	Content	Default
RateMaxECR	1 to $p$ dimensional vector describing the equal concern for the relaxation of the upper constraints on the rate of $u$	0
Name	Name of input signal. This is inherited from InputName of the LTI plant model.	InputName of LTI plant model
Units	String specifying the measurement units for the manipulated variable	' '

---

**Note** Rates refer to the difference  $\Delta u(k)=u(k)-u(k-1)$ . Constraints and weights based on derivatives  $du/dt$  of continuous-time input signals must be properly reformulated for the discrete-time difference  $\Delta u(k)$ , using the approximation  $du/dt \cong \Delta u(k)/T_s$ .

---

**OutputVariables**

OutputVariables (or OV or Controlled or Output) is an  $n_y$ -dimensional array of structures ( $n_y$  = number of outputs), one per output signal. Each structure has the fields described in the following table (Structure OutputVariables on page 3-5), where  $p$  denotes the prediction horizon.

**Structure OutputVariables**

Field Name	Content	Default
Min	1 to $p$ dimensional vector of lower constraints on an output $y$	-Inf
Max	1 to $p$ dimensional vector of upper constraints on an output $y$	Inf

**Structure OutputVariables (Continued)**

Field Name	Content	Default
MinECR	1 to $p$ dimensional vector describing the equal concern for the relaxation of the lower constraints on an output $y$	1
MaxECR	1 to $p$ dimensional vector describing the equal concern for the relaxation of the upper constraints on an output $y$	1
Name	Name of output signal. This is inherited from OutputName of the LTI plant model.	OutputName of LTI plant model
Units	String specifying the measurement units for the measured output	' '
Integrator	Magnitude of integrated white noise on the output channel (0=no integrator)	[]

In order to reject constant disturbances due for instance to gain nonlinearities, the default output disturbance model used in Model Predictive Control Toolbox software is a collection of integrators driven by white noise on measured outputs (see “Output Disturbance Model”). Output integrators are added according to the following rule:

- 1** Measured outputs are ordered by decreasing output weight (in case of time-varying weights, the sum of the absolute values over time is considered for each output channel, and in case of equal output weight, the order within the output vector is followed).
- 2** By following such order, an output integrator is added per measured outputs, unless there is a violation of observability, or you force it by zeroing the corresponding value in `OutputVariables.Integrators`.



By default, `OutputVariables.Integrators` is empty on all outputs. This enforces the default action of Model Predictive Control Toolbox software, namely add integrators on measured outputs, do not add integrators on unmeasured outputs. By setting the entry of `OutputVariables(i).Integrators` to zero, no attempt will be made to add integrated white noise on the  $i$ -th output. On the contrary, by setting the entry of `OutputVariables(i).Integrators` to one, an attempt will be made to add integrated white noise on the  $i$ -th output (see `getoutdist`).

### DisturbanceVariables

`DisturbanceVariables` (or DV or Disturbance) is an  $(n_v+n_d)$ -dimensional array of structures ( $n_v$  = number of measured input disturbances,  $n_d$  = number of unmeasured input disturbances), one per input disturbance. Each structure has the fields described in the following table (Structure `DisturbanceVariables` on page 3-6).

#### Structure `DisturbanceVariables`

Field Name	Content	Default
Name	Name of input signal. This is inherited from <code>InputName</code> of the LTI plant model.	<code>InputName</code> of LTI plant model
Units	String specifying the measurement units for the manipulated variable	''

The order of the disturbance signals within the array `DisturbanceVariables` is the following: the first  $n_v$  entries relate to measured input disturbances, the last  $n_d$  entries relate to unmeasured input disturbances.

---

**Note** The Name properties of ManipulatedVariables, OutputVariables, and DisturbanceVariables are read only. You can set signal names in the Model.Plant.InputName and Model.Plant.OutputName properties of the MPC object, for instance by using the method setname.

---

## Weights

Weights is the structure defining the QP weighting matrices. Unlike the InputSpecs and OutputSpecs, which are arrays of structures, W is a single structure containing four fields. The values of these fields depend on whether you are using the standard quadratic cost function (see “Standard Form”) or the alternative cost function (see “Alternative Cost Function”).

### Standard Cost Function

The table below, Weights for the Standard Cost Function (MATLAB® Structure) on page 3-7, lists the content of the four fields where  $p$  denotes the prediction horizon,  $n_u$  the number of manipulated variables,  $n_y$  the number of output variables.

The fields ManipulatedVariables, ManipulatedVariablesRate, and OutputVariables are arrays with  $n_u$ ,  $n_u$ , and  $n_y$  columns, respectively. If weights are time invariant, then ManipulatedVariables, ManipulatedVariablesRate, and OutputVariables are row vectors. However, for time-varying weights, each field is a matrix with up to  $p$  rows. If the number of rows is less than the prediction horizon,  $p$ , the object constructor duplicates the last row to create a matrix with  $p$  rows.

### Weights for the Standard Cost Function (MATLAB Structure)

Field Name	Content	Default
ManipulatedVariables (or MV or Manipulated or Input)	(1 to $p$ )-by- $n_u$ dimensional array of input weights	zeros(1, $n_u$ )
ManipulatedVariablesRate (or MVRate or ManipulatedRate or InputRate)	(1 to $p$ )-by- $n_u$ dimensional array of input-rate weights	0.1*ones(1, $n_u$ )

**Weights for the Standard Cost Function (MATLAB Structure) (Continued)**

Field Name	Content	Default
OutputVariables (or OV or Controlled or Output)	(1 to $p$ )-by- $n_y$ dimensional array of output weights	1 (The default for output weights is the following: if $n_u \geq n_y$ , all outputs are weighted with unit weight; if $n_u < n_y$ , $n_u$ outputs are weighted with unit weight (with preference given to measured outputs), while the remaining outputs receive zero weight.)
ECR	Weight on the slack variable $\epsilon$ used for softening the constraints	$1e5 * (\text{max weight})$

The default ECR weight is  $10^5$  times the largest weight specified in ManipulatedVariables, ManipulatedVariablesRate, and OutputVariables.

---

**Note** All weights must be greater than or equal to zero. If all weights on manipulated variable increments are strictly positive, the resulting QP problem is always strictly convex. If some of those weights are zero, the Hessian matrix of the QP problem may become only positive semidefinite. In order to keep the QP problem always strictly convex, if the condition number of the Hessian matrix  $K_{\Delta U}$  is larger than  $10^{12}$ , the quantity  $10 * \text{sqrt}(\text{eps})$  is added on each diagonal term. This may only occur when all input rates are not weighted ( $W^{\Delta u} = 0$ ) (see “Cost Function”).

---

### Alternative Cost Function

You can specify off-diagonal  $Q$  and  $R$  weight matrices in the cost function. To accomplish this, you must define the fields `ManipulatedVariables`, `ManipulatedVariablesRate`, and `OutputVariables` as cell arrays, each containing a single positive-semi-definite matrix of the appropriate size. Specifically, `OutputVariables` must be a cell array containing the  $n_y$ -by- $n_y$   $Q$  matrix, `ManipulatedVariables` must be a cell array containing the  $n_u$ -by- $n_u$   $R_u$  matrix, and `ManipulatedVariablesRate` must be a cell array containing the  $n_u$ -by- $n_u$   $R_{\Delta u}$  matrix (see “Alternative Cost Function”) and the `mpcweightsdemo` example). You can abbreviate the field names as shown in `Weights` for the Standard Cost Function (MATLAB® Structure) on page 3-7. You can also use diagonal weights (as defined in `Weights` for the Standard Cost Function (MATLAB® Structure) on page 3-7) for one or more of these fields. If you omit a field, the object constructor uses the defaults shown in `Weights` for the Standard Cost Function (MATLAB® Structure) on page 3-7.

For example, you can specify off-diagonal weights, as follows

```
MPCObj.Weights.OutputVariables={Q};  
MPCObj.Weights.ManipulatedVariables={Ru};  
MPCObj.Weights.ManipulatedVariablesRate={Rdu};
```

where  $Q=Q$ ,  $Ru=R_u$ , and  $Rdu = R_{\Delta u}$  are positive semidefinite matrices.

---

**Note** You cannot specify off-diagonal time-varying weights.

---

### Model

The property `Model` specifies plant, input disturbance, and output noise models, and nominal conditions, according to the model setup described in “State Estimation”. It is specified through a structure containing the fields reported in `Structure Model Describing the Models Used by MPC` on page 3-9.

### Structure Model Describing the Models Used by MPC

Field Name	Content	Default
Plant	LTI model or identified linear model of the plant	No default
Disturbance	LTI model describing color of input disturbances	An integrator on each Unmeasured input channel
Noise	LTI model describing color of plant output measurement noise	Unit white noise on each measured output = identity static gain
Nominal	Structure containing the state, input, and output values where <code>Model.Plant</code> is linearized	See Nominal Values at Operating Point on page 3-11.

---

**Note** Direct feedthrough from manipulated variables to any output in `Model.Plant` is not allowed. See “Prediction Model”.

---

The type of input and output signals is assigned either through the `InputGroup` and `OutputGroup` properties of `Model.Plant`, or, more conveniently, through function `setmpcsignals`, according to the nomenclature described in Input Groups in Plant Model on page 3-10 and Output Groups in Plant Model on page 3-11.

### Input Groups in Plant Model

Name	Value
ManipulatedVariables (or MV or Manipulated or Input)	Indices of manipulated variables
MeasuredDisturbances (or MD or Measured)	Indices of measured disturbances
UnmeasuredDisturbances (or UD or Unmeasured)	Indices of unmeasured disturbances

### Output Groups in Plant Model

Name	Value
MeasuredOutputs (or MO or Measured)	Indices of measured outputs
UnmeasuredOutputs (or UO or Unmeasured)	Indices of unmeasured outputs

By default, all inputs are manipulated variables, and all outputs are measured.

---

**Note** With this current release, the `InputGroup` and `OutputGroup` properties of LTI objects are defined as structures, rather than cell arrays (see the Control System Toolbox™ documentation for more details).

---

The structure `Nominal` contains the nominal values for states, inputs, outputs and state derivatives/differences at the operating point where `Model.Plant` was linearized. The fields are reported in `Nominal Values at Operating Point` on page 3-11 (see “Offsets”).

### Nominal Values at Operating Point

Field	Description	Default
X	Plant state at operating point	0
U	Plant input at operating point, including manipulated variables, measured and unmeasured disturbances	0
Y	Plant output at operating point	0
DX	For continuous-time models, DX is the state derivative at operating point: $DX=f(X,U)$ . For discrete-time models, $DX=x(k+1)-x(k)=f(X,U)-X$ .	0

### Ts

Sampling time of the MPC controller. By default, if `Model.Plant` is a discrete-time model,  $Ts=Model.Plant.ts$ . For continuous-time plant models, you must specify a sampling time for the MPC controller.

### Optimizer

Parameters for the QP optimization. `Optimizer` is a structure with the fields reported in the following table (Optimizer Properties on page 3-12).

#### Optimizer Properties

Field	Description	Default
MaxIter	Maximum number of iterations allowed in the QP solver	200
Trace	On/off	'off'
Solver	QP solver used (only 'ActiveSet')	'ActiveSet'
MinOutputECR	Minimum positive value allowed for <code>OutputMinECR</code> and <code>OutputMaxECR</code>	1e-10

`MinOutputECR` is a positive scalar used to specify the minimum allowed ECR for output constraints. If values smaller than `MinOutputECR` are provided in the `OutputVariables` property of the MPC objects a warning message is issued and the value is raised to `MinOutputECR`.

## **PredictionHorizon**

`PredictionHorizon` is an integer value expressing the number  $p$  of sampling steps of prediction.

## **ControlHorizon**

`ControlHorizon` is either a number of free control moves, or a vector of blocking moves (see “Optimization Variables”).

## **History**

`History` stores the time the MPC controller was created.

## **Notes**

`Notes` stores text or comments as a cell array of strings.

## **UserData**

Any additional data stored within the MPC controller object.

## **MPCData**

`MPCData` is a private property of the MPC object used for storing intermediate operations, QP matrices, internal flags, etc.

## **Version**

`Version` is a private property indicating the Model Predictive Control Toolbox version number.

## **Examples**

Define an MPC controller based on the transfer function model  $s+1/(s^2+2s)$ , with sampling time  $T_s=0.1$  s, and satisfying the input constraint  $-1 \leq u \leq 1$ :

```
Ts=.1;    %Sampling time
MV=struct('Min',-1,'Max',1);
p=20;
```



```
m=3;  
mpc1=mpc(tf([1 1],[1 2 0]),Ts,p,m,[],MV);
```

**See Also**

set | get

# mpchelp

---

**Purpose** MPC property and function help

**Syntax**

```
mpchelp
mpchelp name
out=mpchelp(`name`)
mpchelp(obj)
mpchelp(obj, 'name')
out=mpchelp(obj, 'name')
```

**Description** mpchelp provides a complete listing of Model Predictive Control Toolbox help.

mpchelp name provides online help for the function or property name.

out=mpchelp(`name`) returns the help text in string, out.

mpchelp(obj) displays a complete listing of functions and properties for the MPC object, obj, along with the online help for the object's constructor.

mpchelp(obj, 'name') displays the help for function or property, name, for the MPC object, obj.

out=mpchelp(obj, 'name') returns the help text in string, out.

**Examples** To get help on the MPC method getoutdist, you can type:

```
mpchelp getoutdist
```

**See Also** mpcprops

**Purpose**

Optimal control action

**Syntax**

```
u = mpcmove(MPCobj,x,ym,r,v)
[u,Info] = mpcmove(MPCobj,x,ym,r,v)
[u,Info] = mpcmove(MPCobj,x,ym,r,v,Options)
```

**Description**

`u = mpcmove(MPCobj,x,ym,r,v)` computes the optimal manipulated variable moves,  $u(k)$ .  $u(k)$  is calculated given the current estimated extended state,  $x(k)$ , the measured plant outputs,  $y_m(k)$ , the output references,  $r(k)$ , and the measured disturbances,  $v(k)$ , at time  $k$ . Call `mpcmove` repeatedly to simulate closed-loop model predictive control.

`[u,Info] = mpcmove(MPCobj,x,ym,r,v)` returns additional information regarding the model predictive controller in the second output argument `Info`.

`[u,Info] = mpcmove(MPCobj,x,ym,r,v,Options)` overrides default constraints and weights settings in `MPCobj` with the values specified by `Options`, an `mpcmoveopt` object. Use `Options` to provide run-time adjustment in constraints and weights during the closed-loop simulation.

**Tips**

- `mpcmove` updates `x`.
- If `ym`, `r` or `v` is specified as `[]`, `mpcmove` uses the appropriate `MPCobj.Model.Nominal` value instead.
- To view the predicted optimal behavior for the entire prediction horizon, plot the appropriate sequences provided in `Info`.
- To determine the optimization status, check `Info.Iterations` and `Info.QPCode`.

**Input Arguments**

**MPCobj**

mpc object that defines the model predictive controller.

**x**

mpcstate object that contains the following:

- Estimated plant model states,  $x(k | k-1)$
- Estimated input and output disturbance model states,  $x_d(k | k-1)$
- Estimated measurement noise model states,  $x_m(k | k-1)$
- Last controller moves,  $u(k-1)$

To initialize  $x$ , use  $x = \text{mpcstate}(\text{MPCobj})$  and modify default properties as needed.

You may need to change the value of  $x$  before using it at the next time step under certain circumstances. Suppose that the optimal value for  $u$  calculated in the previous call to `mpcmove` was not used in the plant for some reason (e.g., saturation). You must replace `LastMove` with the values actually used.

`mpcmove` updates all four properties of  $x$  to prepare for an `mpcmove` call at the next time step. For example, it copies the recommended  $u$  values into the `LastMove` field.

To retain the original contents of  $x$ , create a copy of it before calling `mpcmove`.

## **ym**

1-by- $n_{ym}$  vector of current measured output values at time  $k$ .

$n_{ym}$  is the number of measured outputs.

## **r**

$p$ -by- $n_y$  array of future reference values for the outputs, where  $p$  is the prediction horizon and  $n_y$  is the number of outputs. The  $i^{\text{th}}$  row of  $r$  defines the reference values at time  $k+i$ , for  $i = 1, \dots, p$ .

The first row must contain the reference signal at time  $k+1$ . Additional rows represent known future references and are optional (future values are unknown in most applications). If you supply fewer than  $p$  rows of data, `mpcmove` duplicates the last row to fill the array.

You cannot preview the reference signal (also referred to as look-ahead and anticipation) if  $\mathbf{r}$  contains a single row. To support reference previewing, supply at least two rows of data for  $\mathbf{r}$ .

#### **v**

$p$ -by- $n_{md}$  array of current and future measured disturbance, where  $p$  is the prediction horizon and  $n_{md}$  is the number of measured disturbances used in feed-forward control. The  $i^{th}$  row of  $\mathbf{v}$  defines the measured disturbance values at time  $k+i-1$ , for  $i = 1, \dots, p$ .

The first row must contain the current measured disturbance values. Additional rows represent known future values and are optional (future values are unknown in most applications). If you supply fewer than  $p$  rows of data, `mpcmove` duplicates the last row to fill the array.

You cannot preview the measured disturbance signal (also referred to as look-ahead and anticipation) if  $\mathbf{v}$  contains a single row. To support disturbance previewing, supply at least two rows of data for  $\mathbf{v}$ .

#### **Options**

`mpcmoveopt` object that overrides constraints and weights in `MPCobj`. This approach is computationally efficient to simulate run-time changes in controller tuning and limit values. The same behavior can be found in a Simulink® MPC Controller block when supplied with controller tuning and limit input signals.

## **Output Arguments**

#### **u**

1-by- $n_u$  array of optimal manipulated variable moves, where  $n_u$  is the number of manipulated variables.

`mpcmove` holds  $\mathbf{u}$  at its most recent successful solution if the QP solver fails to find a solution for the current time  $k$ .

#### **Info**

Information regarding the model predictive controller.

`Info` is a structure with the following fields:

- $U_{opt}$  —  $p+1$ -by- $n_u$  array containing the optimal manipulated variable adjustments (moves), where  $p$  is the prediction horizon and  $n_u$  is the number of manipulated variables.

The first row is the same as  $u$ , which is to be applied at the current time  $k$ .  $U_{opt}(i, :)$  contains the predicted optimal values at time  $k+i-1$ , for  $i = 1, \dots, p+1$ .

mpcmove does not calculate optimal control moves at time  $k+p$  and therefore it sets  $U_{opt}(p+1, :)$  to NaN.

- $Y_{opt}$  —  $p+1$ -by- $n_y$  array containing the predicted output variable sequence, where  $p$  is the prediction horizon and  $n_y$  is the number of outputs.

The first row contains the current outputs at time  $k$  after state estimation.  $Y_{opt}(i, :)$  contains the values at time  $k+i-1$ , for  $i = 1, \dots, p+1$ .

- $X_{opt}$  —  $p+1$ -by- $n_x$  array containing the predicted state variable sequence, where  $p$  is the prediction horizon and  $n_x$  is the number of states.

The first row contains the current states at time  $k$  as determined by state estimation.  $X_{opt}(i, :)$  contains the values at time  $k+i-1$ , for  $i = 1, \dots, p+1$ .

- $T_{opt}$  —  $p+1$ -by-1 vector of time intervals where  $T_{opt}(1)=0$  (representing the current time) and  $T_{opt}(i)=Ts*(i-1)$ , where  $Ts=MPCObj.Ts$ , the controller sample time and for  $i = 1, \dots, p+1$ .

Use when plotting  $U_{opt}$ ,  $Y_{opt}$  and/or  $X_{opt}$  sequences.

- $Slack$  — Slack variable,  $\varepsilon$ , used in constraint softening.

Slack is a scalar that may have the following values:

- 0 — All constraints were satisfied for the entire prediction horizon
- $>0$  — At least one soft constraint is violated and represents the worst-case soft constraint violation (scaled by your ECR values for each constraint) when more than one constraints are violated.

See “Optimization Problem” for details.

- **Iterations** — QP solution result.

**Iterations** is a scalar integer that may have the following values:

- `>0` — Number of iterations needed to solve the quadratic programming (QP) problem that determines the optimal sequences.
- `0` — QP problem could not be solved in the allowed maximum number of iterations.
- `-1` — QP problem was infeasible. A QP problem is infeasible if no solution can satisfy all the hard constraints.
- `-2` — Numerical error occurred when solving the QP problem.

- **QPCode** — QP solution status.

**QPCode** is a String that may have the following values:

- `'feasible'` — Optimal solution was obtained (`Iterations > 0`)
- `'infeasible'` — QP solver detected a problem with no feasible solution (`Iterations = -1`) or a numerical error occurred (`Iterations = -2`)
- `'unreliable'` — QP solver failed to converge (`Iterations = 0`)

- **Cost** — Cost of the objective function.

**Cost** quantifies the degree to which the controller has achieved its objectives and is a non-negative scalar value. **Cost** is only meaningful when **QPCode** is `'feasible'`.

See “Optimization Problem” for details.

## Examples

### Analyze Closed-Loop Response

Perform closed-loop simulation of a plant with one MV and one measured OV.

Define a plant model and create a model predictive controller with MV constraints.

```
ts = 2;
Plant = ss(0.8,0.5,0.25,0,ts);
MPCobj = mpc(Plant);
MPCobj.MV(1).Min = -2;
MPCobj.MV(1).Max = 2;

-->The "PredictionHorizon" property of "mpc" object is empty. Trying Pred
-->The "ControlHorizon" property of the "mpc" object is empty. Assuming 2
-->The "Weights.ManipulatedVariables" property of "mpc" object is empty.
-->The "Weights.ManipulatedVariablesRate" property of "mpc" object is emp
-->The "Weights.OutputVariables" property of "mpc" object is empty. Assum
```

Initialize an `mpcstate` object for simulation. Use the default state properties.

```
x = mpcstate(MPCobj);

-->Integrated white noise added on measured output channel #1.
-->The "Model.Noise" property of the "mpc" object is empty. Assuming whit
```

Set the reference signal. There is no measured disturbance.

```
r = 1;
```

Simulate the closed-loop response by calling `mpcmove` iteratively.

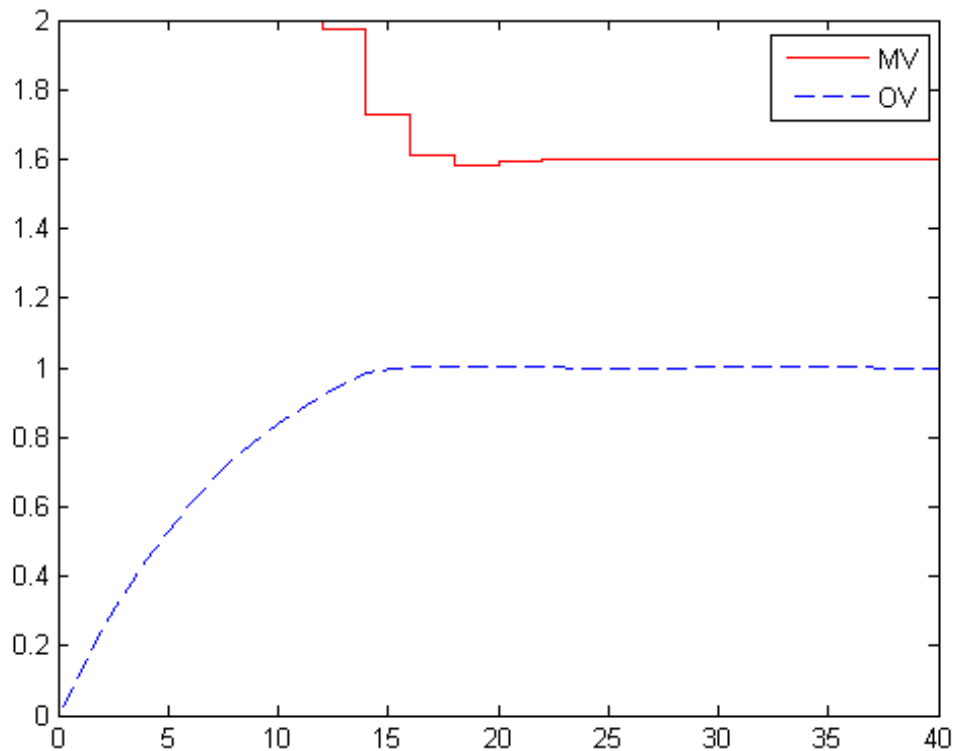
```
t = [0:ts:40];
N = length(t);
y = zeros(N,1);
u = zeros(N,1);
for i = 1:N
    % simulated plant and predictive model are identical
    y(i) = 0.25*x.Plant;
    u(i) = mpcmove(MPCobj,x,y(i),r);
end
```

`y` and `u` store the OV and MV values.



Analyze the result.

```
[ts,us] = stairs(t,u);  
plot(ts,us,'r-',t,y,'b--');  
legend('MV','OV');
```



Modify the MV upper bound as the simulation proceeds using an `mpcmoveopt` object.

```
MPCopt = mpcmoveopt;
```

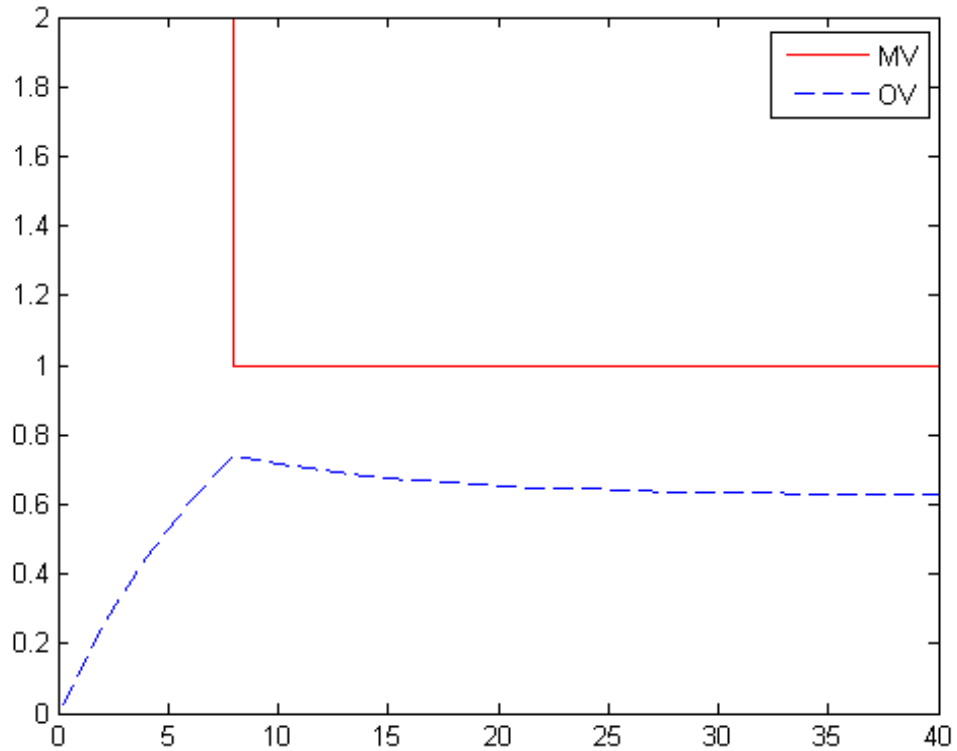
```
MPCopt.MVMin = -2;  
MPCopt.MVMax = 2;
```

Simulate the closed-loop response and introduce the real-time upper limit change at eight seconds (the fifth iteration step).

```
x = mpcstate(MPCobj);  
y = zeros(N,1);  
u = zeros(N,1);  
for i=1:N  
    % simulated plant and predictive model are identical  
    y(i) = 0.25*x.Plant;  
    if i == 5  
        MPCopt.MVMax = 1;  
    end  
    u(i) = mpcmove(MPCobj,x,y(i),r,[],MPCopt);  
end
```

Analyze the result.

```
[ts,us] = stairs(t,u);  
plot(ts,us,'r-',t,y,'b--');  
legend('MV','OV');
```



### Evaluate Scenario at Specific Time Instant

Define a plant model.

```
ts = 2;  
Plant = ss(0.8,0.5,0.25,0,ts);
```

Create a model predictive controller with MV and MVRate constraints. The prediction horizon is ten intervals. The control horizon is blocked.

```
MPCobj = mpc(Plant, ts, 10, [2 3 5]);
MPCobj.MV(1).Min = -2;
MPCobj.MV(1).Max = 2;
MPCobj.MV(1).RateMin = -1;
MPCobj.MV(1).RateMax = 1;
```

```
-->The "Weights.ManipulatedVariables" property of "mpc" object is empty.
-->The "Weights.ManipulatedVariablesRate" property of "mpc" object is empty.
-->The "Weights.OutputVariables" property of "mpc" object is empty. Assuming
```

Initialize an mpcstate object for simulation from a particular state.

```
x = mpcstate(MPCobj);
x.Plant = 2.8;
x.LastMove = 0.85;
```

```
-->Integrated white noise added on measured output channel #1.
-->The "Model.Noise" property of the "mpc" object is empty. Assuming white
```

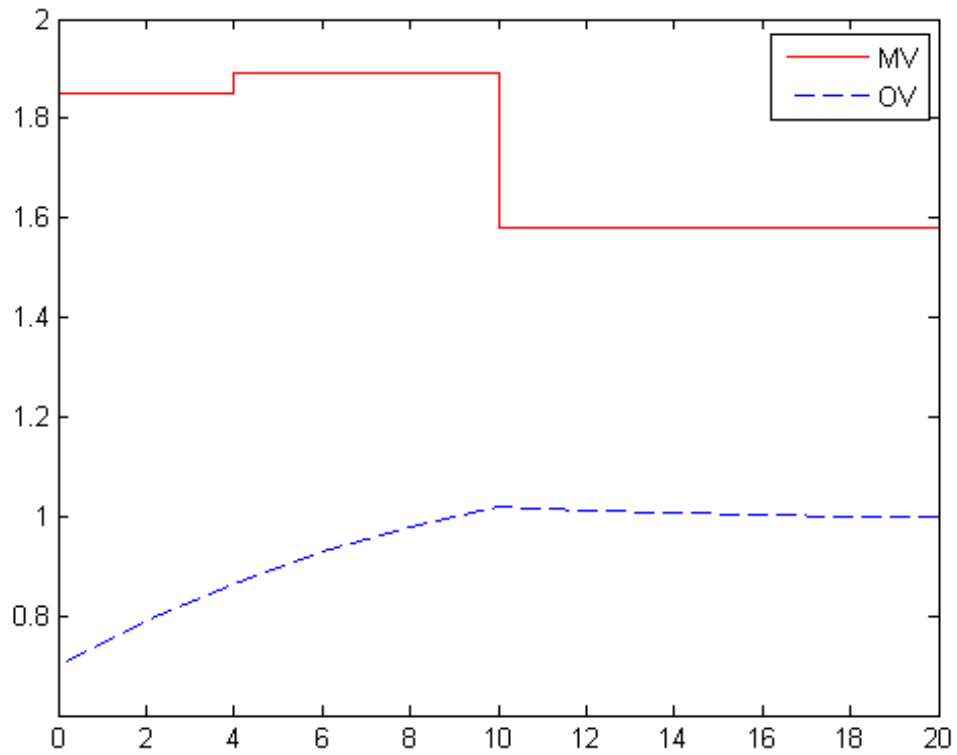
Compute the optimal control at current time.

```
y = 0.25*x.Plant;
r = 1;
[u,Info] = mpcmove(MPCobj,x,y,r);
```

```
-->Integrated white noise added on measured output channel #1.
-->The "Model.Noise" property of the "mpc" object is empty. Assuming white
```

Analyze the predicted optimal sequences.

```
[ts,us] = stairs(Info.Topt,Info.Uopt);
plot(ts,us,'r-',Info.Topt,Info.Yopt,'b--');
legend('MV','OV');
```



plot ignores `Info.Uopt(end)` as it is NaN.

Examine the optimal cost.

`Info.Cost`

ans =

0.0793

## Alternatives

- Use `sim` for plant mismatch and noise simulation when not using run-time constraints or weight changes.
- Use `mpctool` to graphically and interactively combine model predictive design and simulation.
- Use the MPC Controller block in Simulink and for code generation.

## See Also

`mpc` | `mpcmoveopt` | `mpcstate` | `review` | `sim` | `setestim` | `getestim`

## Tutorials

- MPC Control with Anticipative Action (Look-Ahead)
- MPC Control with Input Quantization Based on Comparing the Optimal Costs
- Analysis of Control Sequences Optimized by MPC on a Double Integrator System

**Purpose** Options set for mpcmove

**Syntax** `options = mpcmoveopt`

**Description** `options = mpcmoveopt` creates an `mpcmoveopt` object, with default values for its properties. Use this object with `mpcmove` to allow run-time adjustment of the weights and constraints of the Model Predictive Controller, an `mpc` object, that is operating.

- Tips**
- The number of manipulated variables ( $n_u$ ) and output variables ( $n_y$ ) for the `mpcmoveopt` object must match that of the corresponding `mpc` object.
  - If any weight property in `options` is set to `[]` (default), `mpcmove` uses the corresponding weight specified in the `mpc` object.
  - In general, constraint specifications of `options` must be consistent with those of the corresponding `mpc` object.

If all of the four constraint properties of `options` are set to `[]` (default), `mpcmove` uses the existing constraints specified for the corresponding `mpc` object. The result will be the same as if there are no run-time constraint changes.

Otherwise:

- Constraints set to `[]` are treated as unbounded signals. The corresponding constraint settings for the `mpc` object must also be unbounded.
- Constraints not set to `[]` are treated as bounded signals. The corresponding constraint settings for the `mpc` object must also be bounded.

These requirements make the Model Predictive Controller object behave consistently with the corresponding MPC Controller block in Simulink

A conflict may arise when you have a mixture of bounded and unbounded variables for one or more constraint properties of

`options`. It may be resolved by defining compatible constraints for the `mpc` object and corresponding `mpcmoveopt` object.

For example, suppose  $n_y = 2$ , and your `mpc` object defines a maximum for the first output variable but the second has no upper bound. If,

- `options.OutputMax = []`, then `mpcmove` interprets this as an attempt to remove the upper bound on the first output.
- `options.OutputMax` is not `[]`, then, because all entries must be finite, `mpcmove` interprets this as an attempt to impose a new upper bound on the second output.

To avoid this conflict, modify your `mpc` object to have a large but finite upper bound on the second output. It can then be paired with `options`, containing finite `OutputMax` values, without conflict.

## Output Arguments

### `options`

Options for the `mpcmove` command with the following fields:

- `OutputWeights` — 1-by- $n_y$  vector of output variable tuning weights, where  $n_y$  is the number of output variables. `mpcmove` replaces the `Weight.OutputVariables` field of the corresponding `mpc` object with this vector. The weights must be finite and real values.
- `MVRateWeights` — 1-by- $n_u$  vector of manipulated variable rate tuning weights, where  $n_u$  is the number of manipulated variables. `mpcmove` replaces the `Weight.ManipulatedVariablesRate` field of the corresponding `mpc` object with this vector. The weights must be finite and real values.
- `ECRWeight` — Scalar weight on the slack variable used for constraint softening. `mpcmove` replaces the `Weight.ECR` field of the corresponding `mpc` object with this value. The weight must be a finite and real value.
- `OutputMin` — 1-by- $n_y$  vector of lower bounds on the output variables, where  $n_y$  is the number of output variables. `mpcmove` replaces the `OutputVariables(i).Min` field of the corresponding `mpc` object with this vector, for  $i = 1, \dots, n_y$ .



- **OutputMax** — 1-by- $n_y$  vector of upper bounds on the output variables, where  $n_y$  is the number of output variables. `mpcmove` replaces the `OutputVariables(i).Max` field of the corresponding mpc object with this vector, for  $i = 1, \dots, n_y$ .
- **MVMin** — 1-by- $n_u$  vector of lower bounds on the manipulated variables, where  $n_u$  is the number of manipulated variables. `mpcmove` replaces the `ManipulatedVariables(i).Min` field of the corresponding mpc object with this vector, for  $i = 1, \dots, n_u$ .
- **MVMax** — 1-by- $n_u$  vector of upper bounds on the manipulated variables, where  $n_u$  is the number of manipulated variables. `mpcmove` replaces the `ManipulatedVariables(i).Max` field of the corresponding mpc object with this vector, for  $i = 1, \dots, n_u$ .
- **OnlyComputeCost** — Logical value to control whether the optimal sequence is to be calculated and exported.
  - 0 (default) sets `mpcmove` to compute and return the optimal cost and the optimal sequence of the Model Predictive Controller objective function.
  - 1 sets `mpcmove` to compute and return only the optimal cost of the Model Predictive Controller objective function.

## Examples

Use an `mpcmoveopt` object to vary an MV upper bound during a simulation employing `mpcmove`. The upper bound decreases step-wise from 2 to 1 when elapsed time exceeds 4 seconds. Also, setting `OnlyComputeCost = 1` causes the `Info` object returned by `mpcmove` to contain the cost only.

Define an `mpcmoveopt` object and initialize some of its fields.

```
OPTobj = mpcmoveopt;
OPTobj.OnlyComputeCost = true;
OPTobj.MVMin = -2;
```

Define a plant model and a model predictive controller object.

```
ts = 2;
```

## mpcmoveopt

---

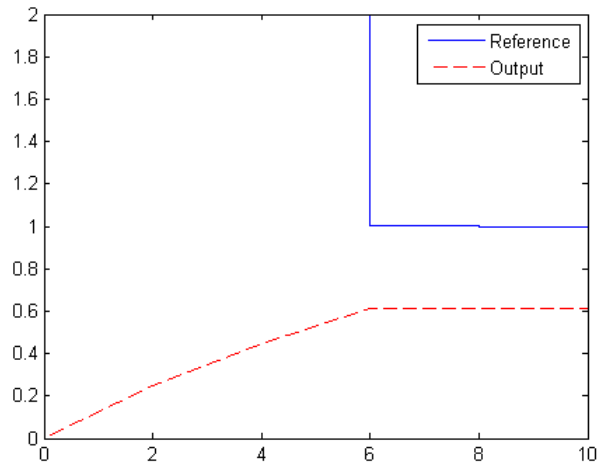
```
Plant = ss(0.8, 0.5, 0.25, 0, ts);
MPCobj = mpc(Plant, ts);
MPCobj.MV(1).Min = -2;
MPCobj.MV(1).Max = 2;
```

Perform mpcmove simulation.

```
x = mpcstate(MPCobj);
r = 1;
v = [];
t = [0:ts:10];
N = length(t);
y = zeros(N,1);
u = zeros(N,1);
for i = 1:N
    y(i) = 0.25*x.Plant;
    % Use the MPCMOVEOPT object to modify the MV upper bound in
    % real time.
    if t(i) <= 4
        OPTobj.MVMax = 2;
    else
        OPTobj.MVMax = 1;
    end
    [u(i), Info] = mpcmove(MPCobj, x, y(i), r, v, OPTobj);
end
```

Analyze the results.

```
[ts, us] = stairs(t, u);
plot(ts, us, 'b-', t, y, 'r--')
legend('Reference', 'Output');
```



## Alternatives

When you use `mpcmove`, an `mpcmoveopt` object is optional. As an alternative, you can modify the weight, constraint definitions, or both before calling `mpcmove`. This approach is usually less computationally efficient, but it avoids potential conflicts with constraint definitions when mixed bounded and unbounded variables are present.

## See Also

`mpc` | `mpcmove` | `setconstraint` | `setterminal`

# mpcprops

---

<b>Purpose</b>	Provide help on MPC controller's properties
<b>Syntax</b>	<code>mpcprops</code>
<b>Description</b>	<code>mpcprops</code> displays details on the generic properties of MPC controllers. It provides a complete list of all the fields of MPC objects with a brief description of each field and the corresponding default values.
<b>See Also</b>	<code>set</code>   <code>get</code>   <code>mpchelp</code>

**Purpose** MPC simulation options

**Syntax** `SimOptions=mpcsimopt(mpcobj)`

**Description** `mpcsimopt` creates an `mpcsimopt` object for specifying additional parameters for simulation with `sim`.

`SimOptions=mpcsimopt(mpcobj)` creates an empty object `SimOptions` which is compatible with the MPC object `mpcobj`. You must use `set / get` to change simulation options.

**Properties** **MPC Simulation Options Properties**

Property	Description
<code>PlantInitialState</code>	Initial state vector of the plant model generating the data.
<code>ControllerInitialState</code>	Initial condition of the MPC controller. This must be a valid <code>@mpcstate</code> object.  <b>Note</b> Nonzero values of <code>ControllerInitialState.LastMove</code> are only meaningful if there are constraints on the increments of the manipulated variables.
<code>UnmeasuredDisturbance</code>	Unmeasured disturbance signal entering the plant.  An array with as many columns as unmeasured disturbances.

## MPC Simulation Options Properties (Continued)

Property	Description
InputNoise	Noise on manipulated variables.  An array with as many columns as manipulated variables. The last sample of the array is extended constantly over the horizon to obtain the correct size.
OutputNoise	Noise on measured outputs.  An array with as many columns as measured outputs. The last sample of the array is extended constantly over the horizon to obtain the correct size.
RefLookAhead	Preview on reference signal ('on' or 'off').
MDLookAhead	Preview on measured disturbance signal ('on' or 'off').
Constraints	Use MPC constraints ('on' or 'off').
Model	Model used in simulation for generating the data.  This property is useful for simulating the MPC controller under model mismatch. The LTI object specified in <code>Model</code> can be either a replacement for <code>Model.Plant</code> , or a structure with fields <code>Plant</code> and <code>Nominal</code> . By default, <code>Model</code> is equal to <code>MPCobj.Model</code> (no model mismatch). If <code>Model</code> is specified, then <code>PlantInitialState</code> refers to the initial state of <code>Model.Plant</code> and is defaulted to <code>Model.Nominal.x</code> .

**MPC Simulation Options Properties (Continued)**

Property	Description
	If Model.Nominal is empty, Model.Nominal.U and Model.Nominal.Y are inherited from MPCObj.Model.Nominal. Model.Nominal.X/DX is only inherited if both plants are state-space objects with the same state dimension.
StatusBar	Display the wait bar ('on' or 'off').
MVSignal	Sequence of manipulated variables (with offsets) for open-loop simulation (no MPC action).  An array with as many columns as manipulated variables.
OpenLoop	Perform open-loop simulation.

**Examples**

We want to simulate the MPC control of a multi-input multi-output (MIMO) system under predicted / actual plant model mismatch. The system has two manipulated variables, two unmeasured disturbances, and two measured outputs.

```
% Open-loop system parameters
p1 = tf(1,[1 2 1])*[1 1; 0 1];
plant = ss([p1 p1]);

% Define I/O types
plant=setmpcsignals(plant,'MV',[1 2],'UD',[3 4]);

% Define I/O names (optional)
set(plant,'InputName',{'mv1','mv2','umd3','umd4'});

% Model for unmeasured input disturbances
```

```
distModel = eye(2,2)*ss(-.5,1,1,0);

% Create MPC object
mpcobj = mpc(plant,1,40,2);
mpcobj.Model.Disturbance = distModel;

% Closed-loop MPC simulation with model mismatch
% and unforeseen unmeasured disturbance inputs

% Define plant model generating the data
p2 = tf(1.5,[0.1 1 2 1])*[1 1; 0 1];
psim = ss([p2 p2 tf(1,[1 1])*[0;1]]);
psim=setmpcsignals(psim,'MV',[1 2],'UD',[3 4 5]);

% Closed-loop simulation
dist=ones(1,3); % Unmeasured disturbance trajectory
refs=[1 2]; % Output reference trajectory
Tf=100; % Total number of simulation steps

options=mpcsimopt(mpcobj);
options.unmeas=dist;
options.model=psim;

sim(mpcobj,Tf,refs,options);
```

## See Also

`sim`



**Purpose**

Define MPC controller state

**Syntax**

```
xmpc = mpcstate(MPCobj, xp, xd, xn, u)
xmpc = mpcstate(MPCobj)
xmpc = mpcstate
```

**Description**

`xmpc = mpcstate(MPCobj, xp, xd, xn, u)` defines an `mpcstate` object for state estimation and optimization in an MPC control algorithm based on the MPC object `MPCobj`. The state of an MPC controller contains the estimates of the states  $x(k)$ ,  $x_d(k)$ ,  $x_m(k)$ , where  $x(k)$  is the state of the plant model,  $x_d(k)$  is the overall state of the input and output disturbance model,  $x_m(k)$  is the state of the measurement noise model, and the value of the last vector  $u(k-1)$  of manipulated variables. The overall state is updated from the measured output  $ym(k)$  by a linear state observer (see “State Observer”).

`xmpc = mpcstate(MPCobj)` returns a default extended initial state that is compatible with the MPC controller `MPCobj`. Such a default state has plant state and previous input initialized at nominal values, and the states of the disturbance and noise models at zero.

Note that `mpcstate` objects are updated by `mpcmove` through the internal state observer based on the extended prediction model.

`xmpc = mpcstate` returns an empty `mpcstate` object.

**Properties**

The `mpcstate` object type contains the state of an MPC controller. Its properties are listed in MPC State Object Properties on page 3-16.

## MPC State Object Properties

Property	Description
Plant	Array of plant states. Values are absolute, i.e., they include possible state offsets (cf. <code>Model.Nominal.X</code> ).
Disturbance	Array of states of unmeasured disturbance models. This contains the states of the input disturbance model and, appended below, the states of the unmeasured output disturbances model.
Noise	Array of states of measurement noise model.
LastInput	Array of previous manipulated variables $u(k-1)$ . Values are absolute, i.e., they include possible input offsets (cf. <code>Model.Nominal.U</code> ).

The command

```
mpcstate(mpcobj)
```

returns a zero extended initial state compatible with the MPC object `mpcobj`, and with `mpcobj.Plant` and `mpcobj.LastInput` initialized at the nominal values specified in `mpcobj.Model.Nominal`.

### See Also

```
getoutdist | setoutdist | setindist | getestim | setestim | ss  
| mpcmove
```

**Purpose** Start Model Predictive Controller GUI

**Syntax**

```
mpctool
mpctool(MPCobj)
mpctool(MPCobj, 'objname')
mpctool(MPCobj1, MPCobj2, ...)
mpctool(MPCobj1, 'objname1', MPCobj2, 'objname2', ...)
mpctool('TaskName')
```

**Description** `mpctool` starts the GUI. For more information about designing and testing model predictive controllers, see “Working with the Design Tool”.

`mpctool(MPCobj)` starts the GUI and loads `MPCobj`, which is an existing controller object.

`mpctool(MPCobj, 'objname')` assigns `objname` (specified as a string) to the controller you are loading into the GUI. If you do not specify a name, the GUI uses the name of the variable that stores the controller object.

`mpctool(MPCobj1, MPCobj2, ...)` loads the specified list of controllers.

`mpctool(MPCobj1, 'objname1', MPCobj2, 'objname2', ...)` loads the specified list of controllers and assigns each controller the specified name.

`mpctool('TaskName')` starts the GUI and creates a new Model Predictive Control design task with the name specified by the string `'TaskName'`.

**See Also** `mpc`

# mpcverbosity

---

**Purpose** Change toolbox verbosity level

**Syntax** `mpcverbosity on`  
`mpcverbosity off`  
`old_status = mpcverbosity(new_status)`  
`mpcverbosity`

**Description** `mpcverbosity on` enables messages displaying default operations taken by Model Predictive Control Toolbox software during the creation and manipulation of model predictive control objects.

`mpcverbosity off` turns messages off.

`old_status = mpcverbosity(new_status)` sets the verbosity level to the specified value, `new_status`. The function returns the original value of the verbosity level as `old_status`. Specify `new_status` as a string with the value of either 'on' or 'off' .

`mpcverbosity` just shows the verbosity status.

By default, messages are turned on.

See also “Construction and Initialization” on page 3-13 .

**See Also** `mpc`

**Purpose** Reduce size of MPC object in memory

---

**Note** pack will be removed in a future version.

---

**Syntax** pack (MPCobj)

**Description** pack (MPCobj) cleans up information build at initialization and stored in the MPCData field of the MPC object MPCobj. This reduces the amount of bytes in memory required to store the MPC object. For MPC objects based on large prediction models, it is recommended to pack the object before saving the object to file, in order to minimize the size of the file.

**See Also** mpc | getmpcdata | setmpcdata | compare

# plot

---

**Purpose** Plot responses generated by MPC simulations

**Syntax** `plot(MPCobj,t,y,r,u,v,d)`

**Description** `plot(MPCobj,t,y,r,u,v,d)` plots the results of a simulation based on the MPC object `MPCobj`. `t` is a vector of length `Nt` of time values, `y` is a matrix of output responses of size `[Nt,Ny]` where `Ny` is the number of outputs, `r` is a matrix of setpoints and has the same size as `y`, `u` is a matrix of manipulated variable inputs of size `[Nt,Nu]` where `Nu` is the number of manipulated variables, `v` is a matrix of measured disturbance inputs of size `[Nt,Nv]` where `Nv` is the number of measured disturbance inputs, and `d` is a matrix of unmeasured disturbance inputs of size `[Nt,Nd]` where `Nd` is the number of unmeasured disturbances input.

**See Also** `sim` | `mpc`

**Purpose** Solve convex quadratic program using Dantzig-Wolfe's algorithm

---

**Note** qpDantz will be removed in a future version. Use quadprog (requires Optimization Toolbox™) instead.

---

**Syntax** `[xopt,lambda,how]=qpDantz(H,f,A,b,xmin)`  
`[xopt,lambda,how]=qpDantz(H,f,A,b,xmin,maxiter)`

**Description** `[xopt,lambda,how]=qpDantz(H,f,A,b,xmin)` solves the convex quadratic program

$$\min \frac{1}{2} x^T H x + f^T x$$

subject to  $Ax \leq b, x \geq x_{min}$

using Dantzig-Wolfe's active set method [2]. The Hessian matrix H should be positive definite. By default, `xmin=1e-3`. Vector `xopt` is the optimizer. Vector `lambda` contains the optimal dual variables (Lagrange multipliers).

The exit flag `how` is either 'feasible', 'infeasible' or 'unreliable'. The latter occurs when the solver terminates because the maximum number `maxiter` of allowed iterations was exceeded.

The solver is implemented in `qpsolver.mex`. Dantzig-Wolfe's algorithm uses the direction of the largest gradient, and the optimum is usually found after about  $n+q$  iterations, where  $n=\dim(x)$  is the number of optimization variables, and  $q=\dim(b)$  is the number of constraints. More than  $3(n+q)$  iterations are rarely required (see Chapter 7.3 of [2]).

**Examples** Solve a random QP problem using quadprog from the Optimization Toolbox software and qpDantz.

```
n=50;      % Number of vars
H=rand(n,n);H=H'*H;H=(H+H')/2;
```

```
f=rand(n,1);
A=[eye(n);-eye(n)];
b=[rand(n,1);rand(n,1)];
x1=quadprog(H,f,A,b,[],[],-100,[],[],...
optimset('LargeScale','off','Algorithm','active-set'));
[x2,how]=qpdantz(H,f,A,b,-100*ones(n,1));
```

## References

- [1] Fletcher, R. Practical Methods of Optimization, John Wiley & Sons, Chichester, UK, 1987.
- [2] Dantzig, G.B. Linear Programming and Extensions, Princeton University Press, Princeton, 1963.



---

<b>Purpose</b>	Examine MPC controller for design errors and stability problems at run-time
<b>Syntax</b>	<code>review(mpcobj)</code>
<b>Description</b>	<p><code>review(mpcobj)</code> checks for potential design issues in the Model Predictive Controller <code>mpcobj</code> and generates a report. <code>review</code> performs the following diagnostic tests:</p> <ul style="list-style-type: none"><li>• Is the optimization problem to be solved online well defined?</li><li>• Is the controller internally stable?</li><li>• Is the closed loop system stable when no constraints are active and there is no model mismatch?</li><li>• Is the controller able to eliminate steady-state tracking error when no constraints are active?</li><li>• Is there a likelihood that constraint definitions will result in an ill-conditioned or infeasible optimization problem?</li></ul>
<b>Tips</b>	<ul style="list-style-type: none"><li>• Use <code>review</code> iteratively to check your initial MPC design or whenever you make substantial changes to <code>mpcobj</code>. Make the recommended changes to your controller to eliminate potential problems.</li><li>• If you design your controller using MPC Design Tool, export the controller to the MATLAB Workspace, and analyze it using <code>review</code>.</li><li>• <code>review</code> does not modify <code>mpcobj</code>.</li><li>• <code>review</code> cannot detect all possible performance factors. So, additionally test your design using techniques such as simulations.</li></ul>
<b>Input Arguments</b>	<p><b><code>mpcobj</code></b> Non-empty Model Predictive Controller (mpc) object</p>
<b>Examples</b>	Create a Model Predictive Controller with hard upper and lower bounds on the manipulated variable and its rate-of-change.

Create a discrete Model Predictive Controller.

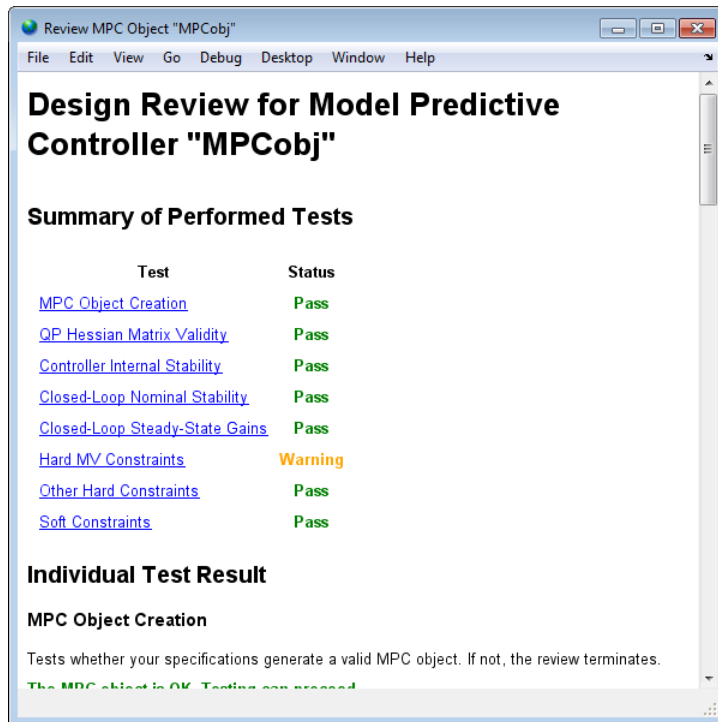
```
% Create a Model Predictive Controller
Plant = tf(1, [10 1]);
ts = 2;
MPCobj = mpc(Plant,ts);
```

Specify hard bounds on the MV and its rate of change.

```
MV = MPCobj.MV;
MV.Min = -2;
MV.Max = 2;
MV.RateMin = -4;
MV.RateMax = 4;
MPCobj.MV = MV;
```

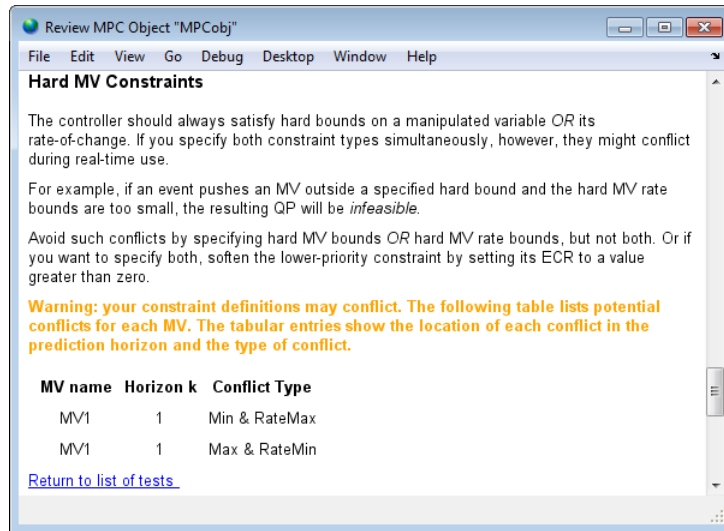
Review the design.

```
review(MPCobj)
```



review flags the potential constraint conflict that could result if you applied this controller to a real process.

Examine the warning by clicking **Hard MV Constraints**.



## Alternatives

review automates certain tests that you could perform yourself.

To test for steady-state tracking errors, use `cloffset`.

To test the internal stability of a controller, check the eigenvalues of the `mpc` object. Use `ss` to convert the `mpc` object to a state-space model and call `isstable`.

## See Also

`cloffset` | `mpc` | `ss`

## Tutorials

- Reviewing Model Predictive Controller Design for Potential Stability and Robustness Issues
- “Simulation and Code Generation Using Simulink Coder”

## Purpose

Compute effect of controller tuning weights on performance

## Syntax

```
[J, sens] = sensitivity(MPCObj, PerfFunc, PerfWeights, Tstop, r, v,
    simopt, utarget)
[J, sens] = sensitivity(MPCObj, 'perf_fun', param1, param2, ...)
```

## Description

The sensitivity function is a controller tuning aid.  $J$  specifies a scalar performance metric. `sensitivity` computes  $J$  and its partial derivatives with respect to the controller tuning weights. These *sensitivities* suggest tuning weight adjustments that should improve performance, i.e., reduce  $J$ .

`[J, sens] = sensitivity(MPCObj, PerfFunc, PerfWeights, Tstop, r, v, simopt, utarget)` calculates the scalar performance metric,  $J$ , and sensitivities, `sens`, for the controller defined by the MPC controller object `MPCObj`.

`PerfFunc` must be one of the following strings:

'ISE' (integral squared error) for which the performance metric is

$$J = \sum_{i=1}^{Tstop} \left( \sum_{j=1}^{n_y} (w_j^y e_{yij})^2 + \sum_{j=1}^{n_u} [(w_j^u e_{uij})^2 + (w_j^{\Delta u} \Delta u_{ij})^2] \right)$$

'IAE' (integral absolute error) for which the performance metric is

$$J = \sum_{i=1}^{Tstop} \left( \sum_{j=1}^{n_y} |w_j^y e_{yij}| + \sum_{j=1}^{n_u} (|w_j^u e_{uij}| + |w_j^{\Delta u} \Delta u_{ij}|) \right)$$

'ITSE' (integral of time-weighted squared error) for which the performance metric is

$$J = \sum_{i=1}^{Tstop} i \Delta t \left( \sum_{j=1}^{n_y} (w_j^y e_{yij})^2 + \sum_{j=1}^{n_u} [(w_j^u e_{uij})^2 + (w_j^{\Delta u} \Delta u_{ij})^2] \right)$$

$$J = \sum_{i=1}^{Tstop} i\Delta t \left( \sum_{j=1}^{n_y} |w_j^y e_{yij}| + \sum_{j=1}^{n_u} (|w_j^u e_{uij}| + |w_j^{\Delta u} \Delta u_{ij}|) \right)$$

'ITAE' (integral of time-weighted absolute error) for which the performance metric is

In the above expressions  $n_y$  is the number of controlled outputs and  $n_u$  is the number of manipulated variables.  $e_{yij}$  is the difference between output  $j$  and its setpoint (or reference) value at time interval  $i$ .  $e_{uij}$  is the difference between manipulated variable  $j$  and its target at time interval  $i$ .

The  $w$  parameters are non-negative performance weights defined by the structure PerfWeights, which contains the following fields:

'OutputVariables': 1 by  $n_y$  vector containing the  $w_j^y$  values

'ManipulatedVariables': 1 by  $n_u$  vector containing the  $w_j^u$  values

'ManipulatedVariablesRate': 1 by  $n_u$  vector containing the  $w_j^{\Delta u}$  values

If PerfWeights is unspecified, it defaults to the corresponding weights in MPCObj. In general, however, the performance weights and those used in the controller have different purposes and should be defined accordingly.

Inputs Tstop, r, v, and simopt define the simulation scenario used to evaluate performance. See sim for details.

Tstop is the integer number of controller sampling intervals to be simulated. The final time for the simulations will be  $Tstop \times \Delta t$ , where  $\Delta t$  is the controller sampling interval specified in MPCObj.

The optional input utarget is a vector of  $n_u$  manipulated variable targets. Their defaults are the nominal values of the manipulated variables.  $\Delta u_{ij}$  is the change in manipulated variable  $j$  and its target at time interval  $i$ .

The structure variable `sens` contains the computed sensitivities (partial derivatives of `J` with respect to the `MPCobj` tuning weights.) Its fields are

'OutputVariables'	(1 by $n_y$ ) sensitivities with respect to <code>MPCobj.Weights.OutputVariables</code>
'ManipulatedVariables'	(1 by $n_u$ ) sensitivities with respect to <code>MPCobj.Weights.ManipulatedVariables</code>
'ManipulatedVariablesRate'	(1 by $n_u$ ) sensitivities with respect to <code>MPCobj.Weights.ManipulatedVariablesRate</code>

See “Weights” on page 3-7 for details on the tuning weights contained in `MPCobj`.

```
[J, sens] =
sensitivity(MPCobj, 'perf_fun', param1, param2, ...) employs a
performance function 'perf_fun' to define J. Its function definition
must be in the form
```

```
function J = perf_fun(MPCobj, param1, param2, ...)
```

i.e., it must compute `J` for the given controller and optional parameters `param1`, `param2`, ... and it must be on the MATLAB path.

---

**Note** While performing the sensitivity analysis, the software ignores time-varying, nondiagonal, and ECR slack variable weights.

---

## Examples

Suppose variable `MPCobj` contains a default controller definition for a plant with two controlled outputs, three manipulated variables, and no measured disturbances. Compute its performance and sensitivities as follows:

```
PerfFunc = 'IAE';
PerfWts.OutputVariables = [1 0.5];
PerfWts.ManipulatedVariables = zeros(1,3);
PerfWts.ManipulatedVariablesRate = zeros(1,3);
Tstop = 20;
```

# sensitivity

---

```
r = [1 0];  
v = [];  
simopt = mpcsimopt;  
utarget = zeros(1,3);  
[J, sens] = sensitivity(MPCobj, PerfFunc, PerfWts, Tstop, ...  
    r, v, simopt, utarget)
```

The simulation scenario in the above example uses a constant  $r = 1$  for output 1 and  $r = 0$  for output 2. In other words, the scenario is a unit step in the output 1 setpoint.

## See Also

[mpc](#) | [sim](#)



**Purpose**

Set or modify MPC object properties

**Syntax**

```
set(MPCobj, 'Property', Value)
set(MPCobj, 'Property1', Value1, 'Property2', Value2, ...)
set(MPCobj, 'Property')
set(sys)
```

**Description**

The `set` function is used to set or modify the properties of an MPC controller (see “MPC Controller Object” on page 3-2 for background on MPC properties). Like its Handle Graphics® counterpart, `set` uses property name/property value pairs to update property values.

`set(MPCobj, 'Property', Value)` assigns the value `Value` to the property of the MPC controller `MPCobj` specified by the string `'Property'`. This string can be the full property name (for example, `'UserData'`) or any unambiguous case-insensitive abbreviation (for example, `'user'`).

`set(MPCobj, 'Property1', Value1, 'Property2', Value2, ...)` sets multiple property values with a single statement. Each property name/property value pair updates one particular property.

`set(MPCobj, 'Property')` displays admissible values for the property specified by `'Property'`. See “MPC Controller Object” on page 3-2 for an overview of legitimate MPC property values.

`set(sys)` displays all assignable properties of `sys` and their admissible values.

**See Also**

`mpc` | `get` | `mpcprops`

# setconstraint

---

**Purpose** Custom constraints on plant inputs and outputs

**Syntax**  
`setconstraint(MPCobj,E,F,G)`  
`setconstraint(MPCobj,E,F,G,V)`  
`setconstraint(MPCobj,E,F,G,V,S)`

**Description** `setconstraint(MPCobj,E,F,G)` adds constraints of the following form to an MPC controller MPCobj:

$$Eu(k+j|k) + Fy(k+j|k) \leq G$$

where:

$$j = 0, \dots, p$$

$p$  is the prediction horizon length

$y$  are the measured and unmeasured outputs

$u$  are the manipulated variables

$E$ ,  $F$ , and  $G$  are constants. Each row of  $E$ ,  $F$ , and  $G$  represents a linear constraint to be imposed at each prediction horizon step.

`setconstraint(MPCobj,E,F,G,V)` adds constraints of the following form:

$$Eu(k+j|k) + Fy(k+j|k) \leq G + \varepsilon V$$

where,

$V$  is a constant representing the Equal Concern for the Relaxation (ECR)

$\varepsilon$  is the slack variable used for constraint softening (as in Equation 2-3 of "Standard Form")

`setconstraint(MPCobj,E,F,G,V,S)` adds constraints of the following form:

$$Eu(k+j|k) + Fy(k+j|k) + Sv(k+j|k) \leq G + \varepsilon V$$

where:

$v$  are the measured disturbances  
 $S$  is a constant

## Tips

- The outputs  $y$  are being predicted using a model. If the model is imperfect, there is no guarantee that a constraint can be satisfied.
- Because  $u(k + p | k)$  is not optimized by the MPC controller, the last constraint at time  $k + p$  assumes that  $u(k+p | k) = u(k+p-1 | k)$ .

## Input Arguments

### MPCobj

MPC controller, specified as an MPC Controller object

### E

Constant used in custom constraints, specified as a matrix with:

$n_u$  columns, where  $n_u$  is the number of manipulated variables  
 Same number of rows as  $F$ ,  $G$ ,  $V$ , and  $S$

To remove all the mixed constraints, use  $[]$  or zero matrix for both the  $E$  and  $F$  matrices.

### F

Constant used in custom constraints, specified as a matrix with:

$n_y$  columns, where  $n_y$  is the number of controlled outputs (measured and unmeasured)  
 Same number of rows as  $E$ ,  $G$ ,  $V$ , and  $S$

To remove all the mixed constraints, use  $[]$  or zero matrix for both the  $E$  and  $F$  matrices.

### G

Constant used in custom constraints, specified as a column vector with the same number of rows as  $E$ ,  $F$ ,  $V$ , and  $S$ .

### V

# setconstraint

---

Constant used in custom constraints, specified as a column vector with the same number of rows as E, F, G, and S.

If  $V$  is not specified, the default of 1 is applied to all constraint inequalities and all constraints are soft (default behavior for output bounds as described in “Standard Form”).

To make the  $i^{\text{th}}$  constraint hard, specify  $V(i) = 0$ .

To make the  $i^{\text{th}}$  constraint soft, specify  $V(i)(>)0$  in keeping with the constraint violation magnitude you can tolerate. The magnitude violation depends on the numerical scale of the variables involved in the constraint.

In general, as  $V(i)$  decreases, the controller decreases the allowed constraint violation, i.e., the constraint becomes harder.

---

**Note** If a constraint is difficult to satisfy, reducing its  $V(i)$  value (to make it harder) may be counter-productive, and can lead to erratic control action, instability, or failure of the QP solver that determines the control action.

---

**Default:** vector of 1s

## S

Constant used in custom constraints, specified as a matrix with:

$n_v$  columns, where  $n_v$  is the number of measured disturbances  
Same number of rows as E, F, G and V

## Examples

This example shows how to specify the custom constraint  $0 \leq u_2 - 2u_3 + y_2 \leq 15$  on an MPC controller. The controller has three manipulated variables and two controlled outputs.

The constraint imposes upper and lower bounds on  $u_2 - 2u_3 + y_2$ .

**1** Formulate this constraint in the required form:

$$\begin{bmatrix} 0 & -1 & 2 \\ 0 & 1 & -2 \end{bmatrix} \begin{bmatrix} u_1 \\ u_2 \\ u_3 \end{bmatrix} + \begin{bmatrix} 0 & -1 \\ 0 & 1 \end{bmatrix} \begin{bmatrix} y_1 \\ y_2 \end{bmatrix} \leq \begin{bmatrix} 0 \\ 15 \end{bmatrix}$$

**2** Specify the constraints on the plant inputs and outputs:

```
E = [0 -1 2; 0 1 -2];
F = [0 -1; 0 1];
G = [0; 15];
setconstraint(MPCobj, E, F, G);
```

Alternatively, you can use:

```
E = [0 -1 2; 0 1 -2];
F = [0 -1; 0 1];
G = [0; 15];
V = [1; 1];
S = [];
setconstraint(MPCobj, E, F, G, V, S);
```

## See Also

setterminal

## Tutorials

- MPC Control with Constraints on a Combination of Input and Output Signals
- MPC Control of a Nonlinear Blending Process

## How To

- “Custom Constraints on Inputs and Outputs”

# setestim

---

**Purpose** Modify MPC object's linear state estimator

**Syntax** `setestim(MPCobj,M)`  
`setestim(MPCobj,'default')`

**Description** The `setestim` function modifies the linear estimator gain of an MPC object. The state estimator is based on the linear model (see “State Estimation”).

$$x(k+1) = Ax(k) + B_u u(k) + B_v v(k)$$

$$y_m(k) = C_m x(k) + D_{vm} v(k)$$

where  $v(k)$  are the measured disturbances,  $u(k)$  are the manipulated plant inputs,  $y_m(k)$  are the measured plant outputs, and  $x(k)$  is the overall state vector collecting states of plant, unmeasured disturbance, and measurement noise models. The order of the states in  $x$  is the following: plant states; disturbance models states; noise model states.

`setestim(MPCobj,M)`, where `MPCobj` is an MPC object, changes the default Kalman estimator gain stored in `MPCobj` to that specified by matrix `M`.

`setestim(MPCobj,'default')` restores the default Kalman gain.

The estimator used in Model Predictive Control Toolbox software is described in “State Estimation”. The estimator's equations are as follows.

## **Predicted Output Computation:**

$$\hat{y}_m(k|k-1) = C_m \hat{x}(k|k-1) + D_{vm} v(k)$$

## **Measurement Update:**

$$\hat{x}(k|k) = \hat{x}(k|k-1) + M(y_m(k) - \hat{y}_m(k|k-1))$$

**Time Update:**

$$\hat{x}(k+1|k) = A\hat{x}(k|k) + B_u u(k) + B_v v(k)$$

By combining these three equations, the overall state observer is

$$\hat{x}(k+1|k) = (A - LC_m)\hat{x}(k|k-1) + Ly_m(k) + B_u u(k) + (B_v - LD_{vm})v(k)$$

where  $L = AM$ .

---

**Note** The estimator gain  $M$  has the same meaning as the gain  $L$  in the kalman function in Control System Toolbox software.

---

Matrices  $A$ ,  $B_u$ ,  $B_v$ ,  $C_m$ ,  $D_{vm}$  can be retrieved using `getestim` as follows:

```
[M,A,Cm,Bu,Bv,Dvm]=getestim(MPCobj)
```

**Examples****Design State Estimator by Pole Placement**

Design an estimator using pole placement, assuming the linear system  $AM=L$  is solvable.

Create a plant model.

```
G = tf({1,1,1},{[1 .5 1],[1 1],[.7 .5 1]});
```

To improve the clarity of this example, call `mpcverbosity` to suppress messages related to working with an MPC controller.

```
old_status = mpcverbosity('off');
```

Create a model predictive controller for the plant. Specify the controller sample time as 0.2 seconds.

```
MPCobj = mpc(G, 0.2);
```

Obtain the default state estimator gain.

```
[M,A1,Cm1] = getestim(MPCobj);
```

Calculate the default observer poles.

```
e = eig(A1-A1*M*Cm1);  
abs(e)
```

```
ans =
```

```
0.9402  
0.9402  
0.8816  
0.8816  
0.7430  
0.9020
```

Specify faster observer poles.

```
new_poles = [.8 .75 .7 .85 .6 .81];
```

Compute a state-gain matrix that places the observer poles at `new_poles`.

```
L = place(A1',Cm1',new_poles)';
```

`place` returns the controller-gain matrix, whereas you want to compute the observer-gain matrix. Using the principle of duality, which relates controllability to observability, you specify the transpose of `A1` and `Cm1` as the inputs to `place`. This function call yields the observer gain transpose.

Obtain the estimator gain from the state-gain matrix.

```
M=A1\L;
```



Specify M as the estimator for MPCobj.

```
setestim(MPCobj,M);
```

The pair,  $(A_1, C_{m1})$ , describing the overall state-space realization of the combination of plant and disturbance models must be observable for the state estimation design to succeed. Observability is checked in Model Predictive Control Toolbox software at two levels: (1) observability of the plant model is checked *at construction* of the MPC object, provided that the model of the plant is given in state-space form; (2) observability of the overall extended model is checked *at initialization* of the MPC object, after all models have been converted to discrete-time, delay-free, state-space form and combined together.

Restore `mpcverbosity`.

```
mpcverbosity(old_status);
```

## See Also

```
getestim | mpc | mpcstate | kalman
```

# setindist

---

**Purpose** Modify unmeasured input disturbance model

**Syntax** `setindist(MPCobj, 'integrators')`  
`setindist(MPCobj, 'model', model)`

**Description** `setindist(MPCobj, 'integrators')` imposes the default disturbance model for unmeasured inputs, that is, for each unmeasured input disturbance channel, an integrator is added unless there is a violation of observability, otherwise the input is treated as white noise with unit variance (this is equivalent to `MPCobj.Model.Disturbance=[]`).

`setindist(MPCobj, 'model', model)` sets the input disturbance model to `model` (this is equivalent to `MPCobj.Model.Disturbance=model`).

**See Also** `mpc` | `getindist` | `setestim` | `getestim` | `setoutdist`

**Purpose** Set private MPC data structure

---

**Note** setmpcdata will be removed in a future version. Use set, setconstraint, setestim, setindist and setoutdist instead.

---

**Syntax** setmpcdata(MPCobj,mpcdata)

**Description** setmpcdata(MPCobj,mpcdata) changes the private field MPCData of the MPC object MPCobj, where all internal QP matrices, models, estimator gains are stored at initialization of the object. You may only need this for very advanced use of Model Predictive Control Toolbox software.

---

**Note** Changes to the data structure may easily lead to unpredictable results.

---

**See Also** getmpcdata | set | get | pack

# setmpcsignals

---

**Purpose** Set signal types in MPC plant model

**Syntax** `P=setmpcsignals(P,SignalType1,Channels1,SignalType2,Channels2,...)`

**Description** The purpose of `setmpcsignals` is to set I/O channels of the MPC plant model `P`. `P` must be an LTI object. Valid signal types, their abbreviations, and the channel type they refer to are listed below.

Signal Type	Abbreviation	Channel
Manipulated	MV	Input
MeasuredDisturbances	MD	Input
UnmeasuredDisturbances	UD	Input
MeasuredOutputs	MO	Output
UnmeasuredOutputs	UO	Output

Unambiguous abbreviations of signal types are also accepted.

`P=setmpcsignals(P)` sets channel assignments to default, namely all inputs are manipulated variables (MVs), all outputs are measured outputs (MOs). More generally, input signals that are not explicitly assigned are assumed to be MVs, while unassigned output signals are considered as MOs.

## Examples

We want to define an MPC object based on the LTI discrete-time plant model `sys` with four inputs and three outputs. The first and second input are measured disturbances, the third input is an unmeasured disturbance, the fourth input is a manipulated variable (default), the second output is an unmeasured, all other outputs are measured.

```
sys=setmpcsignals(sys,'MD',[1 2],'UD',[3],'UO',[2]);  
mpc1=mpc(sys);
```

---

**Note** When using `setmpcsignals` to modify an existing MPC object, be sure that the fields `Weights`, `MV`, `OV`, `DV`, `Model.Noise`, and `Model.Disturbance` are consistent with the new I/O signal types.

---

## See Also

`mpc` | `set`

# setname

---

**Purpose** Set I/O signal names in MPC prediction model

**Syntax**  
`setname(MPCobj, 'input', I, name)`  
`setname(MPCobj, 'output', I, name)`

**Description** `setname(MPCobj, 'input', I, name)` changes the name of the I-th input signal to name. This is equivalent to `MPCobj.Model.Plant.InputName{I}=name`. Note that `setname` also updates the read-only Name fields of `MPCobj.DisturbanceVariables` and `MPCobj.ManipulatedVariables`.

`setname(MPCobj, 'output', I, name)` changes the name of the I-th output signal to name. This is equivalent to `MPCobj.Model.Plant.OutputName{I} =name`. Note that `setname` also updates the read-only Name field of `MPCobj.OutputVariables`.

---

**Note** The Name properties of `ManipulatedVariables`, `OutputVariables`, and `DisturbanceVariables` are read-only. You must use `setname` to assign signal names, or equivalently modify the `Model.Plant.InputName` and `Model.Plant.OutputName` properties of the MPC object.

---

**See Also** `getname` | `mpc` | `set`

**Purpose**

Modify unmeasured output disturbance model

**Syntax**

```
setoutdist(MPCobj, 'integrators')  
setoutdist(MPCobj, 'remove', channels)  
setoutdist(MPCobj, 'model', model)
```

**Description**

`setoutdist(MPCobj, 'integrators')` specifies the default method output disturbance model, based on the specs stored in `MPCobj.OutputVariables.Integrator` and `MPCobj.Weights.OutputVariables`. Output integrators are added according to the following rules:

- 1** Outputs are ordered by decreasing output weight (in case of time-varying weights, the sum of the absolute values over time is considered for each output channel. In case of equal output weight, the order within the output vector is followed).
- 2** By following such order, an output integrator is added per measured outputs, unless one of the following is true:
  - There is a violation of observability
  - The corresponding value in `MPCobj.OutputVariables.Integrator` is zero
  - The corresponding value in `MPCobj.Weights.OutputVariables` is zero.

A warning is issued when an integrator is added to an unmeasured output channel.

`setoutdist(MPCobj, 'remove', channels)` removes integrators from the output channels specified in vector `channels`. This corresponds to setting `MPCobj.OutputVariables(channels).Integrator=0`. The default for `channels` is `(1:ny)`, where `ny` is the total number of outputs, that is, all output integrators are removed.

`setoutdist(MPCobj, 'model', model)` replaces the array of output integrators designed by default according to

## setoutdist

---

MPCobj.OutputVariables.Integrator with the LTI model `model`. The model must have `ny` outputs. If no model is specified, then the default model based on the specs stored in MPCobj.OutputVariables.Integrator and MPCobj.Weights.OutputVariables is used (same as `setoutdist(MPCobj, 'integrators')`).

### See Also

`mpc` | `getestim` | `setestim` | `setoutdist` | `setindist`



**Purpose** Terminal weights and constraints

**Syntax** `setterminal(MPCobj,Y,U)`  
`setterminal(MPCobj,Y,U,Pt)`

**Description** `setterminal(MPCobj,Y,U)` specifies diagonal quadratic penalty weights and constraints at the last step in the prediction horizon. The weights and constraints are on the terminal output  $y(t+p)$  and terminal input  $u(t+p-1)$ , where  $p$  is the prediction horizon of the MPC controller MPCobj.

`setterminal(MPCobj,Y,U,Pt)` specifies diagonal quadratic penalty weights and constraints from step  $Pt$  to the horizon end. By default,  $Pt$  is the last step in the horizon.

**Tips**

- Advanced users can impose terminal polyhedral state constraints:  
 $K_1 \leq Hx \leq K_2$ .  
 First, augment the plant model with additional artificial (unmeasured) outputs,  $y = Hx$ . Then specify bounds  $K_1$  and  $K_2$  on these  $y$  outputs.

**Input Arguments** **MPCobj**  
 MPC controller, specified as an MPC controller object

**Y**  
 Terminal weights and constraints for the output variables, specified as a structure with the following fields:

Weight	1-by- $n_y$ vector of nonnegative weights
Min	1-by- $n_y$ vector of lower bounds
Max	1-by- $n_y$ vector of upper bounds

MinECR	1-by- $n_y$ vector of constraint-softening Equal Concern for the Relaxation (ECR) values for the lower bounds
MaxECR	1-by- $n_y$ vector of constraint-softening ECR values for the upper bounds

$n_y$  is the number of controlled outputs of the MPC controller.

If the `Weight`, `Min` or `Max` field is empty, the values in `MPCObj` are used at all prediction horizon steps including the last. For the standard bounds, if any element of the `Min` or `Max` field is infinite, the corresponding variable is unconstrained at the terminal step.

Off-diagonal weights are zero (as in Equation 2-3 of “Standard Form”). To apply non-zero off-diagonal terminal weights, you must augment the plant model. See [Implementing Infinite-Horizon LQR by Setting Terminal Weights in a Finite-Horizon MPC Formulation](#).

By default,  $Y.MinECR = Y.MaxECR = 1$  (soft output constraints).

Choose the ECR magnitudes carefully, accounting for the importance of each constraint and the numerical magnitude of a typical violation.

## U

Terminal weights and constraints for the manipulated variables, specified as a structure with the following fields:

Weight	1-by- $n_u$ vector of nonnegative weights
Min	1-by- $n_u$ vector of lower bounds
Max	1-by- $n_u$ vector of upper bounds
MinECR	1-by- $n_u$ vector of constraint-softening Equal Concern for the Relaxation (ECR) values for the lower bounds
MaxECR	1-by- $n_u$ vector of constraint-softening ECR values for the upper bounds

$n_u$  is the number of manipulated variables of the MPC controller.

If the `Weight`, `Min` or `Max` field is empty, the values in `MPCobj` are used at all prediction horizon steps including the last. For the standard bounds, if individual elements of the `Min` or `Max` fields are infinite, the corresponding variable is unconstrained at the terminal step.

Off-diagonal weights are zero (as in Equation 2-3 of “Standard Form”). To apply non-zero off-diagonal terminal weights, you must augment the plant model. See *Implementing Infinite-Horizon LQR by Setting Terminal Weights in a Finite-Horizon MPC Formulation*.

By default, `U.MinECR = U.MaxECR = 0` (hard manipulated variable constraints)

Choose the ECR magnitudes carefully, accounting for the importance of each constraint and the numerical magnitude of a typical violation.

**Pt**

Step in the prediction horizon, specified as an integer between 1 and  $p$ , where  $p$  is the prediction horizon. The terminal values are applied to `Y` and `U` from prediction step `Pt` to the end.

**Default:** Prediction horizon  $p$

**Examples**

This example shows how to specify constraints and a penalty weight at the last step of the prediction horizon of an MPC controller. The controller has three output variables and two manipulated variables.

- 1 Specify a prediction horizon of 8.

```
MPCobj.PredictionHorizon = 8;
```

- 2 Define a penalty weight and constraints:

```
Y=struct('Weight',[1,10,0],'Min',[0,-Inf,-1],...
        'Max',[Inf,2,Inf]);
U=struct('Min',[1,-Inf]);
```

The constraints and weights include:

- Diagonal penalty weights of 1 and 10 on the first two output variables
- Lower bounds of 0 and  $-1$  on outputs 1 and 3, none on output 2
- Upper bound at 2 on output 2, none on outputs 1 and 3
- Lower bound at 1 on manipulated variable 1
- No other conditions (weights or bounds) on the manipulated variables

**3** Specify the constraints and weight at the last step (step 8) of the prediction horizon:

```
setterminal(MPCobj,Y,U);
```

---

This example shows how to specify constraints and a penalty weight beginning with step 5 and ending at the last step of the prediction horizon of an MPC controller. The controller has three output variables and two manipulated variables.

**1** Specify a prediction horizon of 8.

```
MPCobj.PredictionHorizon = 8;
```

**2** Define a penalty weight and constraints:

```
Y=struct('Weight',[1,10,0],'Min',[0,-Inf,-1],...  
        'Max',[Inf,2,Inf]);  
U=struct('Min',[1,-Inf]);
```

The constraints and weights include:

- Diagonal penalty weights of 1 and 10 on the first two output variables
- Lower bounds of 0 and  $-1$  on outputs 1 and 3, none on output 2
- Upper bound at 2 on output 2, none on outputs 1 and 3

- Lower bound at 1 on manipulated variable 1
- No other conditions (weights or bounds) on the manipulated variables

**3** Specify the constraints and weight beginning with step 5 and ending at the last step of the prediction horizon:

```
setterminal(MPCobj,Y,U,5);
```

## See Also

| [mpc](#) | [mpcprops](#) | [setconstraint](#)

## Tutorials

- “Providing LQR Performance Using Terminal Penalty”
- Implementing Infinite-Horizon LQR by Setting Terminal Weights in a Finite-Horizon MPC Formulation

## How To

- “Terminal Weights and Constraints”

**Purpose** Simulate closed-loop/open-loop response to arbitrary reference and disturbance signals

**Syntax**

```
sim(MPCobj,T,r)
sim(MPCobj,T,r,v)
sim(MPCobj,T,r,SimOptions)
sim(MPCobj,T,r,v,SimOptions)
[y,t,u,xp,xmpc,SimOptions] = sim(MPCobj,T,...)
```

**Description** The purpose of `sim` is to simulate the MPC controller in closed loop with a linear time-invariant model, which, by default, is the plant model contained in `MPCobj.Model.Plant`. As an alternative, `sim` can simulate the open-loop behavior of the model of the plant, or the closed-loop behavior in the presence of a model mismatch between the prediction plant model and the model of the process generating the output data.

`sim(MPCobj,T,r)` simulates the closed-loop system formed by the plant model specified in `MPCobj.Model.Plant` and by the MPC controller specified by the MPC object `MPCobj`, and plots the simulation results. `T` is the number of simulation steps. `r` is the reference signal array with as many columns as the number of output variables.

`sim(MPCobj,T,r,v)` also specifies the measured disturbance signal `v`, that has as many columns as the number of measured disturbances.

---

**Note** The last sample of `r/v` is extended constantly over the simulation horizon, to obtain the correct size.

---

`sim(MPCobj,T,r,SimOptions)` specifies the simulation options object `SimOptions`, such as initial states, input/output noise and unmeasured disturbances, plant mismatch, etc. See `mpcsimopt` for details.

`sim(MPCobj,T,r,v,SimOptions)` additionally specifies the measured disturbance signal, `v`.

Without output arguments, `sim` automatically plots input and output trajectories.

`[y,t,u,xp,xmpc,SimOptions] = sim(MPCobj,T,...)` instead of plotting closed-loop trajectories returns the sequence of plant outputs `y`, the time sequence `t` (equally spaced by `MPCobj.Ts`), the sequence `u` of manipulated variables generated by the MPC controller, the sequence `xp` of states of the model of the plant used for simulation, the sequence `xmpc` of states of the MPC controller (provided by the state observer), and the options object `SimOptions` used for the simulation.

The descriptions of the input arguments and their default values are shown in the table below.

Input Argument	Description	Default
<code>MPCobj</code>	MPC object specifying the parameters of the MPC control law	None
<code>T</code>	Number of simulation steps	Largest row-size of <code>r,v,d,n</code>
<code>r</code>	Reference signal	<code>MPCobj.Model.Nominal.Y</code>
<code>v</code>	Measured disturbance signal	Entries from <code>MPCobj.Model.Nominal.U</code>
<code>SimOptions</code>	Object of class <code>@mpcsimopt</code> containing the simulation parameters (See <code>mpcsimopt</code> )	<code>[]</code>

`r` is an array with as many columns as outputs, `v` is an array with as many columns as measured disturbances. The last sample of `r/v/d/n` is extended constantly over the horizon, to obtain the correct size.

The output arguments of `sim` are detailed below.

Output Argument	Description
y	Sequence of controlled plant outputs (without noise added on measured ones)
t	Time sequence (equally spaced by MPCobj.Ts)
u	Sequence of manipulated variables generated by MPC
xp	Sequence of states of plant model (from Model or SimOptions.Model)
xmpc	Sequence of states of MPC controller (estimates of the extended state). This is a structure with the same fields as the mpcstate object.

## Examples

### Simulate MPC Control of MISO Plant

Simulate the MPC control of a MISO system. The system has one manipulated variable, one measured disturbance, one unmeasured disturbance, and one output.

Create the continuous-time plant model. This plant will be used as the prediction model for the MPC controller.

```
sys = ss(tf({1,1,1},{[1 .5 1],[1 1],[.7 .5 1]}));
```

Discretize the plant model using a sampling time of 0.2 units.

```
Ts = 0.2;
sysd = c2d(sys,Ts);
```

Specify the MPC signal type for the plant input signals.

```
sysd = setmpcsignals(sysd, 'MV',1, 'MD',2, 'UD',3);
```

Create an MPC controller for the sysd plant model. Use default values for the weights and horizons.



```
MPCobj = mpc(sysd);
```

```
-->The "PredictionHorizon" property of "mpc" object is empty. Trying P  
-->The "ControlHorizon" property of the "mpc" object is empty. Assumin  
-->The "Weights.ManipulatedVariables" property of "mpc" object is empt  
-->The "Weights.ManipulatedVariablesRate" property of "mpc" object is  
-->The "Weights.OutputVariables" property of "mpc" object is empty. As
```

Constrain the manipulated variable to the [0 1] range.

```
MPCobj.MV = struct('Min',0,'Max',1);
```

Specify the simulation stop time.

```
Tstop = 30;
```

Define the reference signal and the measured disturbance signal.

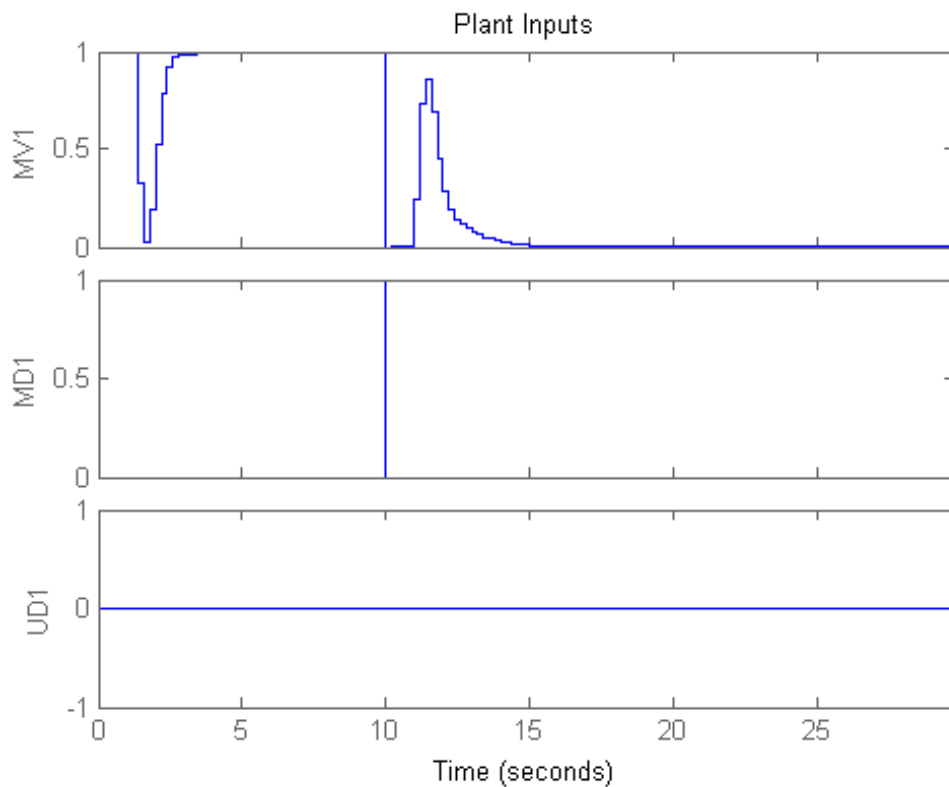
```
num_sim_steps = round(Tstop/Ts);  
r = ones(num_sim_steps,1);  
v = [zeros(num_sim_steps/3,1); ones(2*num_sim_steps/3,1)];
```

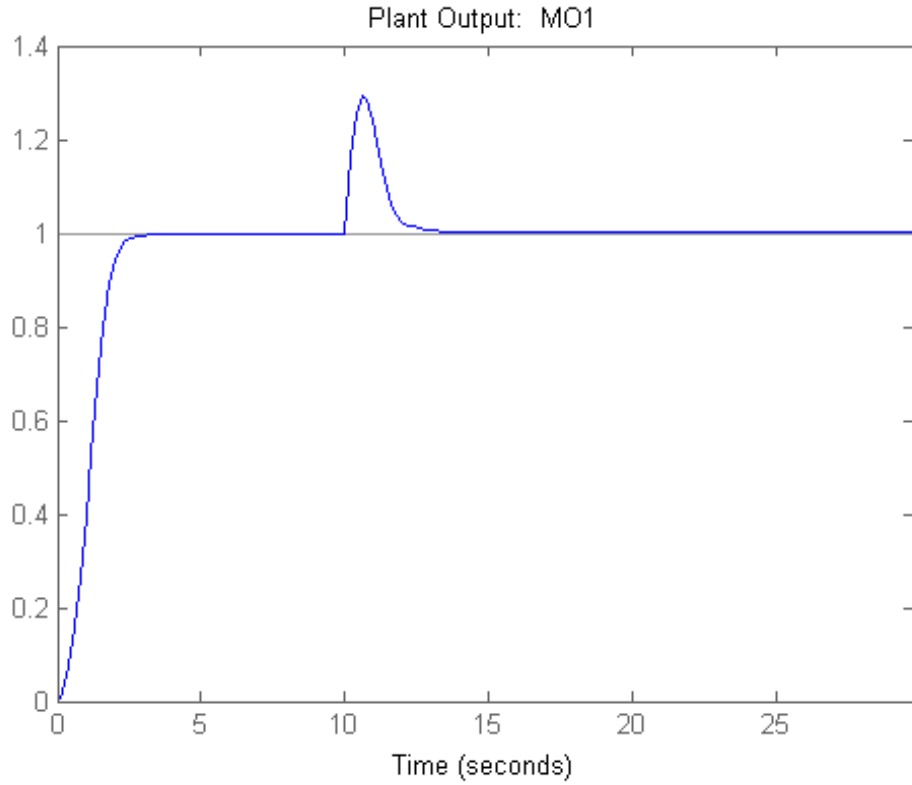
The reference signal,  $r$ , is a unit step. The measured disturbance signal,  $v$ , is a unit step, with a 10 unit delay.

Simulate the controller.

```
sim(MPCobj,num_sim_steps,r,v);
```

```
-->The "Model.Disturbance" property of "mpc" object is empty:  
    Assuming unmeasured input disturbance #3 is integrated white noise.  
-->The "Model.Noise" property of the "mpc" object is empty. Assuming w
```





**See Also** `mpcsimopt` | `mpc` | `mpcmove`

# size

---

**Purpose** Size and order of MPC Controller

**Syntax** `mpc_obj_size = size(MPCobj)`  
`mpc_obj_size = size(MPCobj,signal_type)`  
`size(MPCobj)`

**Description** `mpc_obj_size = size(MPCobj)` returns a row vector specifying the number of manipulated inputs and measured controlled outputs of an MPC controller. This row vector contains the elements  $[n_u \ n_{ym}]$ , where  $n_u$  is the number of manipulated inputs and  $n_{ym}$  is the number of measured controlled outputs.

`mpc_obj_size = size(MPCobj,signal_type)` returns the number of signals of the specified type that are associated with the MPC controller.

You can specify `signal_type` as one of the following strings:

- 'uo' — Unmeasured controlled outputs
- 'md' — Measured disturbances
- 'ud' — Unmeasured disturbances
- 'mv' — Manipulated variables
- 'mo' — Measured controlled outputs

`size(MPCobj)` displays the size information for all the signal types of the MPC controller.

**See Also** `mpc` | `set`

**Purpose** Convert unconstrained MPC controller to state-space linear system

**Syntax**

```
sys=ss(MPCobj)
sys = ss(MPCobj,signals)
sys = ss(MPCobj,signals,ref_preview,md_preview)
[sys,ut] = ss(MPCobj)
```

**Description** The `ss` command returns a linear controller in the state-space form. The controller is equivalent to the MPC controller `MPCobj` when the constraints are not active. The purpose is to use the linear equivalent control in Control System Toolbox software for sensitivity analysis and other linear analysis.

`sys=ss(MPCobj)` returns the linear discrete-time dynamic controller `sys`

$$x(k+1) = Ax(k) + By_m(k)$$

$$u(k) = Cx(k) + Dy_m(k)$$

where  $y_m$  is the vector of measured outputs of the plant, and  $u$  is the vector of manipulated variables. The sampling time of controller `sys` is `MPCobj.Ts`.

---

**Note** Vector  $x$  includes the states of the observer (plant+disturbance+noise model states) and the previous manipulated variable  $u(k-1)$ .

---

`sys = ss(MPCobj,signals)` returns the linearized MPC controller in its full form and allows you to specify the signals that you want to include as inputs for `sys`.

The full form of the MPC controller has the following structure:

$$x(k+1) = Ax(k) + By_m(k) + B_r r(k) + B_v v(k) + B_{ut} u_{target}(k) + B_{off}$$

$$u(k) = Cx(k) + Dy_m(k) + D_r r(k) + D_v v(k) + D_{ut} u_{target}(k) + D_{off}$$

Here,  $r$  is the vector of setpoints for both measured and unmeasured plant outputs,  $v$  is the vector of measured disturbances,  $u_{target}$  is the vector of preferred values for manipulated variables.

Specify `signals` as a single or multicharacter string constructed using any of the following:

- 'r' — Output references
- 'v' — Measured disturbances
- 'o' — Offset terms
- 't' — Input targets

For example, to obtain a controller that maps  $[y_m; r; v]$  to  $u$ , use:

```
sys = ss(MPCobj, 'rv');
```

In the general case of nonzero offsets,  $y_m$  (as well as  $r$ ,  $v$ , and  $u_{target}$ ) must be interpreted as the difference between the vector and the corresponding offset. Offsets can be nonzero if `MPCobj.Model.Nominal.Y` or `MPCobj.Model.Nominal.U` are nonzero.

Vectors  $B_{off}$ ,  $D_{off}$  are constant terms. They are nonzero if and only if `MPCobj.Model.Nominal.DX` is nonzero (continuous-time prediction models), or `MPCobj.Model.Nominal.Dx-MPCobj.Model.Nominal.X` is nonzero (discrete-time prediction models). In other words, when `Nominal.X` represents an equilibrium state,  $B_{off}$ ,  $D_{off}$  are zero.

Only the following fields of `MPCobj` are used when computing the state-space model: `Model`, `PredictionHorizon`, `ControlHorizon`, `Ts`, `Weights`.

`sys = ss(MPCobj, signals, ref_preview, md_preview)` specifies if the MPC controller has preview actions on the reference and measured disturbance signals. If the flag `ref_preview='on'`, then matrices  $B_r$  and  $D_r$  multiply the whole reference sequence:

$$x(k+1) = Ax(k) + By_m(k) + B_r[r(k);r(k+1);...;r(k+p-1)] + \dots$$

$$u(k) = Cx(k) + Dy_m(k) + D_r[r(k);r(k+1);...;r(k+p-1)] + \dots$$

Similarly if the flag `md_preview='on'`, then matrices  $B_v$  and  $D_v$  multiply the whole measured disturbance sequence:

$$x(k+1) = Ax(k) + \dots + B_v[v(k);v(k+1);\dots;v(k+p)] + \dots$$

$$u(k) = Cx(k) + \dots + D_v[v(k);v(k+1);\dots;v(k+p)] + \dots$$

`[sys,ut] = ss(MPCobj)` additionally returns the input target values for the full form of the controller.

`ut` is returned as a vector of doubles, `[utarget(k); utarget(k+1); ... utarget(k+h)]`.

Here:

- $h$  — Maximum length of previewed inputs, that is,  $h = \max(\text{length}(\text{MPCobj.ManipulatedVariables(:)}.Target))$
- `utarget` — Difference between the input target and corresponding input offsets, that is, `MPCobj.ManipulatedVariables(:).Targets - MPCobj.Model.Nominal.U`

## Examples

### Convert Unconstrained MPC Controller to State-Space Model

To improve the clarity of the example, suppress messages about working with an MPC controller.

```
old_status = mpcverbosity('off');
```

Create the plant model.

```
G = rss(5,2,3);
G.D = 0;
G = setmpcsignals(G,'mv',1,'md',2,'ud',3,'mo',1,'uo',2);
```

Configure the MPC controller with nonzero nominal values, weights, and input targets.

```
C = mpc(G,0.1);
C.Model.Nominal.U = [0.7 0.8 0];
C.Model.Nominal.Y = [0.5 0.6];
```

```
C.Model.Nominal.DX = rand(5,1);  
C.Weights.MV = 2;  
C.Weights.OV = [3 4];  
C.MV.Target = [0.1 0.2 0.3];
```

`C` is an unconstrained MPC controller. Specifying `C.Model.Nominal.DX` as nonzero means that the nominal values are not at steady state.

`C.MV.Target` specifies three preview steps.

Covert `C` to a state-space model.

```
sys = ss(C);
```

The output, `sys`, is a seventh-order SISO state-space model. The seven states include the five plant model states, one state from the default input disturbance model, and one state from the previous move,  $u(k-1)$ .

Restore `mpcverbosity`.

```
mpcverbosity(old_status);
```

**See Also**

`mpc` | `set` | `tf` | `zpk`



---

<b>Purpose</b>	Convert unconstrained MPC controller to linear transfer function
<b>Syntax</b>	<code>sys=tf(MPCobj)</code>
<b>Description</b>	The <code>tf</code> function computes the transfer function of the linear controller <code>ss(MPCobj)</code> as an LTI system in <code>tf</code> form corresponding to the MPC controller when the constraints are not active. The purpose is to use the linear equivalent control in Control System Toolbox software for sensitivity and other linear analysis.
<b>See Also</b>	<code>ss</code>   <code>zpk</code>

# trim

---

**Purpose** Compute steady-state value of MPC controller state for given inputs and outputs

**Syntax** `x = trim(MPCobj,y,u)`

**Description** The trim function finds a steady-state value for the plant state or the best approximation in a least squares sense such that:

$$x - x_{off} = A(x - x_{off}) + B(u - u_{off})$$

$$y - y_{off} = C(x - x_{off}) + D(u - u_{off})$$

Here,  $x_{off}$ ,  $u_{off}$ , and  $y_{off}$  are the nominal values of the extended state  $x$ , input  $u$ , and output  $y$ .

`x` is returned as an `mpcstate` object. Specify `y` and `u` as doubles. `y` specifies the measured and unmeasured output values. `u` specifies the manipulated variable, measured disturbance, and unmeasured disturbance values. The values for unmeasured disturbances must be 0.

`trim` assumes the disturbance model and measurement noise model to be zero when computing the steady-state value. The software uses the extended state vector to perform the calculation.

**See Also** `mpc` | `mpcstate`

<b>Purpose</b>	Convert unconstrained MPC controller to zero/pole/gain form
<b>Syntax</b>	<code>sys=zpk(MPCobj)</code>
<b>Description</b>	The <code>zpk</code> function computes the zero-pole-gain form of the linear controller <code>ss(MPCobj)</code> as an LTI system in <code>zpk</code> form corresponding to the MPC controller when the constraints are not active. The purpose is to use the linear equivalent control in Control System Toolbox software for sensitivity and other linear analysis.
<b>See Also</b>	<code>ss</code>   <code>tf</code>



# Block Reference

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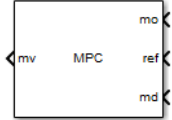
# MPC Controller

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**Purpose** Compute MPC control law

**Library** MPC Simulink Library

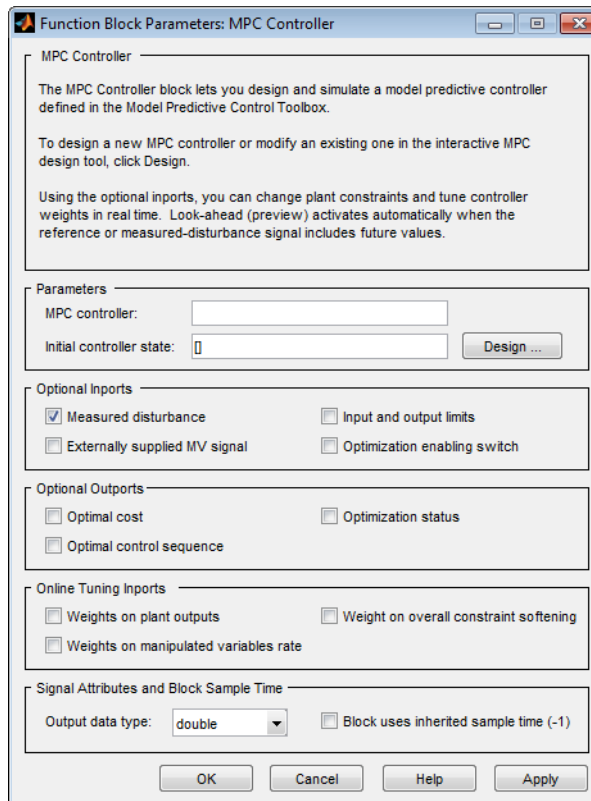
## Description



The MPC Controller block receives the current measured output signal (**mo**), reference signal (**ref**), and optional measured disturbance signal (**md**). The block computes the optimal manipulated variables (**mv**) by solving a quadratic program (QP).

To use the block in simulation and code generation, you must specify an **mpc** object, which defines a model predictive controller. This controller must have already been designed for the plant that it will control.

Because the MPC Controller block uses MATLAB Function blocks to implement the QP solver, it requires compilation each time you change the MPC object and block. Also, because MATLAB does not allow compiled code to reside in any MATLAB product folder, you must use a non-MATLAB folder to work on your Simulink model when you use MPC blocks.



## Dialog Box

The MPC Controller block has the following parameter groupings:

- “Parameters” on page 2-4
- “Required Inports” on page 2-5
- “Required Outports” on page 2-6
- “Optional Inports” on page 2-6
- “Optional Outports” on page 2-10
- “Online Tuning Inports” on page 2-12

# MPC Controller

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- “Signal Attributes and Block Sample Time” on page 2-14

## Parameters

### MPC controller

You must provide an `mpc` object that defines your controller using one of the following methods:

- Enter the name of an `mpc` object in the **MPC Controller** edit box. This object must be present in the base workspace.

Clicking **Design** opens the MPC design tool where you can modify the controller settings in a graphical environment. For example, you can:

- Import a new prediction model.
- Change horizons, constraints, and weights.
- Evaluate MPC performance with a linear plant.
- Export the updated controller to the base workspace.

To see how well the controller works for the nonlinear plant, run a closed-loop Simulink simulation.

- If you do not have an existing `mpc` object in the base workspace, leave the **MPC controller** field empty and, with the MPC Controller block connected to the plant, click **Design**. This action constructs a default `mpc` controller by obtaining a linearized model from the Simulink diagram at the default operating point. Continue your controller design in the MPC design tool.

To use this design approach, you must have Simulink Control Design™ software.

### Initial controller state

Specifies the initial controller state. If this parameter is left blank, the block uses the nominal values that are defined in the `Model.Nominal` property of the `mpc` object. To override the default, create an `mpcstate` object in your workspace that represents the initial state, and enter its name in the field.



## Required Inports

### Measured output

At each control instant, the `mo` signal must contain the current output variable measurements. Let  $n_{ym}$  be the number of measured output variables (MO) defined in your predictive controller. If  $n_{ym}=1$ , connect a scalar signal to the `mo` inport. Otherwise, connect a row or column vector signal containing  $n_{ym}$  real, double-precision elements.

### Reference

At each control instant, the `ref` signal must contain the current reference values (targets or setpoints) for the  $n_y$  output variables ( $n_y = n_{ym} + \text{number of unmeasured outputs}$ ). You have the option to specify future reference values (previewing).

The `ref` signal must be size  $N$  by  $n_y$ , where  $N(1 \leq N \leq p)$  is the number of time steps for which you are specifying reference values and  $p$  is the prediction horizon. Each element must be a real double-precision number. The `ref` dimension must not change from one control instant to the next.

When  $N=1$ , you cannot preview. To specify future reference values, choose  $N$  such that  $1 < N \leq p$  to enable previewing. Doing so usually improves performance via `feedforward` information. The first row specifies the  $n_y$  references for the first step in the prediction horizon (at the next control interval  $k=1$ ), and so on for  $N$  steps. If  $N < p$ , the last row designates constant reference values to be used for the remaining  $p-N$  steps.

For example, suppose  $n_y=2$  and  $p=6$ . At a given control instant, the signal connected to the controller's `ref` inport is

```
[ 2 5    k=1
  2 6    k=2
  2 7    k=3
  2 8]   k=4
```

The signal informs the controller that:

- Reference values for the first prediction horizon step ( $k=1$ ) are 2 and 5.
- The first reference value remains at 2, but the second increases gradually.
- The second reference value becomes 8 at the beginning of the fourth step ( $k=4$ ) in the prediction horizon.
- Both values remain constant at 2 and 8 respectively for steps 5–6 of the prediction horizon.

`mpcpreview` shows how to use reference previewing in a specific case. For calculation details on the use of the reference signal, see “Optimization Problem”.

## Required Outputs

### Manipulated Variables

The `mv` output provides a signal defining the  $n_u \geq 1$  manipulated variables, which are to be implemented in the plant. The controller updates its `mv` output by solving a quadratic program at each control instant. The elements are real, double-precision values.

## Optional Inputs

### Measured disturbance

Add an input (`md`) to which you can connect a measured disturbance signal.

Your measured disturbance signal (`MD`) must be size  $N \times n_{md}$ , where  $n_{md} (\geq 1)$  is the number of measured disturbances defined in your Model Predictive Controller and  $N (1 \leq N \leq p+1)$  is the number of time steps for which the MD is known. Each element must be a real, double-precision number. The signal dimensions must not change from one control instant to the next.

If  $N=1$  you cannot preview. At each control instant, the MD signal must contain the most recent measurements at the current time  $k=0$  (as a row vector, length  $n_{md}$ ). The controller assumes that the MDs remain constant at their current values for the entire prediction horizon.

If you are able to predict future MD values, choose  $N$  such that  $1 < N \leq p+1$  to enable previewing. Doing so usually improves performance via **feedforward**. In this case, the first row must contain the  $n_{md}$  current values at  $k=0$ , and the remaining rows designate variations over the next  $N-1$  control instants. If  $N < p+1$ , the last row designates constant MD values to be used for the remaining  $p+1-N$  steps of the prediction horizon.

For example suppose  $n_{md}=2$  and  $p=6$ . At a given control instant, the signal connected to the controller's md inport is:

```
[2 5      k=0
 2 6      k=1
 2 7      k=2
 2 8]     k=3
```

This signal informs the controller that:

- The current MDs are 2 and 5 at  $k=0$ .
- The first MD remains at 2, but the second increases gradually.
- The second MD becomes 8 at the beginning of the step 3 ( $k=3$ ) in the prediction horizon.
- Both values remain constant at 2 and 8 respectively for steps 4–6 of the prediction horizon.

`mpcpreview` shows how to use MD previewing in a specific case.

For calculation details, see “Prediction Model” and “QP Matrices”.

### **Externally supplied MV signals**

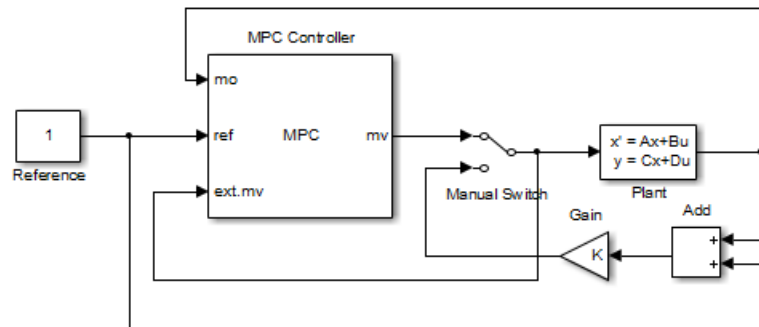
Add an inport (`ext.mv`), which you can connect to the actual manipulated variables (MV) used in the plant. The block uses these to

# MPC Controller

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update its internal state estimates. For example, suppose the actual signals saturate at physical limits or the MV is under manual control. In both cases, feeding the actual value back to the MPC Controller block can improve performance significantly, because the prediction model's state estimates are updated more accurately.

The following example shows how a manual switch may override the controller's output. Also see Turning Controller Online and Offline with Bumpless Transfer.



Do not connect this option to leave the `ext.mv` inport unconnected. In either case, the model predictive controller assumes that the plant uses the MV signals sent by the MPC Controller block. In the preceding example, the external MV signal always provides the model predictive controller that the control signal actually used in the plant. Otherwise, the model predictive controller's internal state estimate would be inaccurate.

---

**Note** The MPC Controller block is a discrete-time block with sampling time inherited from the MPC object. The MPC block has direct feedthrough from measured outputs (`mo`), output references (`ref`), and measured disturbances (`md`) to MPC-manipulated variables (`mv`). There is no direct feedthrough from externally supplied manipulated variables (`ext.mv`) to MPC-manipulated variables (`mv`).

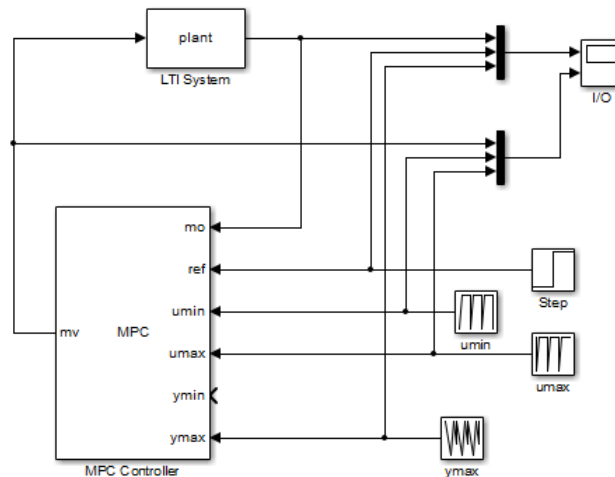
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## Input and output limits

Add inports ( $u_{min}, u_{max}, y_{min}, y_{max}$ ), which you can connect to run-time constraint signals. If this check box is not selected, the block uses the constant constraint values stored within its mpc object. Example connections appear in the following model. See Varying Input and Output Constraints for an example of using this option.

Each unconnected limit inport, such as  $y_{min}$  in the following model, is treated as an unbounded signal. The corresponding constraint settings in the mpc object must also be unbounded. For connected limit inports, such as  $y_{max}$ , the signals must be finite and the corresponding variables in the mpc object must also be bounded.

All constraint signals connected to the block must be finite. Also, you cannot change the number or identity of constrained and unconstrained variables. For example, if your mpc object specifies that your first MV has a lower bound, you must supply a  $u_{min}$  signal for it.



## Optimization enabling switch

Add an inport (QP Switch) whose input specifies whether the controller performs optimization calculations. If the input signal is zero, the

controller behaves normally. If the input signal becomes nonzero, the MPC Controller block turns off the controller's optimization calculations and sets the controller output to zero. These actions save computational effort when the controller output is not needed, such as when the system has been placed in manual operation or another controller has taken over. The controller, however, continues to update its internal state estimate in the usual way. Thus, it is ready to resume optimization calculations whenever the QP Switch signal returns to zero.

If you select this option, the mask automatically selects the **Externally supplied MV signal** option. Connect this option to the current MV value in the plant. Otherwise, there would be a "bump" each time the QP Switch signal reactivates optimization.

## Optional Outputs

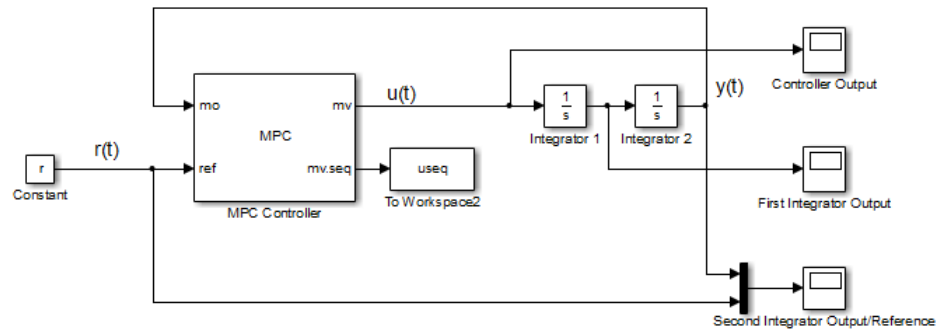
### Optimal cost

Add an output (`cost`) that provides the calculated optimal cost (scalar) of the quadratic program during operation. The computed value is an indication of controller performance. If the controller is performing well, the value is low. However, if the optimization problem is infeasible, this value is meaningless. (See `qp.status`.)

### Optimal control sequence

Add an output (`mv.seq`) that provides the controller's computed optimal MV sequence for the entire prediction horizon from  $k=0$  to  $k=p-1$ . If  $n_u$  is the number of MVs and  $p$  is the length of the prediction horizon, this signal is a  $p$  by  $n_u$  matrix. The first row represents  $k=0$  and duplicates the block's MV output.

The following block diagram (from Analysis of Control Sequences Optimized by MPC on a Double Integrator System) illustrates how to use this option. The diagram shows how to collect diagnostic data and send it to the To Workspace2 block, which creates the variable, `useq`, in the workspace. Run the example to see how the optimal sequence evolves with time.



## Optimization status

Add an output (`qp.status`) that allows you to monitor the status of the QP solver.

If a QP problem is solved successfully at a given control interval, the `qp.status` output returns the number of QP solver iterations used in computation. This value is a finite, positive integer and is proportional to the time required for the calculations. Thus, a large value means a relatively slow block execution at this time interval.

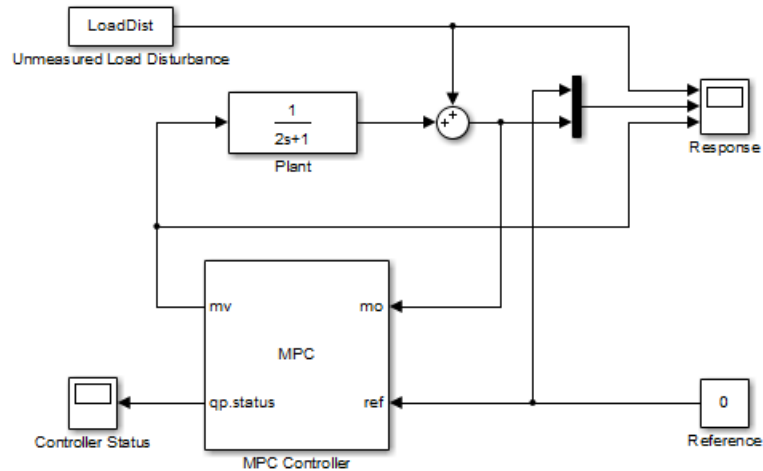
The QP solver may fail to find an optimal solution for the following reasons:

- `qp.status = 0` — The QP solver cannot find a solution within the maximum number of iterations specified in the `mpc` object.
- `qp.status = -1` — The QP solver detects an infeasible QP problem. See [Monitoring Optimization Status to Detect Controller Failures](#) for an example where a large, sustained disturbance drives the OV outside its specified bounds.
- `qp.status = -2` — The QP solver has encountered numerical difficulties in solving a severely ill-conditioned QP problem.

For all the previous three failure modes, the MPC block holds its `mv` output at the most recent successful solution. In a real-time application, you can use status indicator to set an alarm or take other special action.

# MPC Controller

The next diagram shows how to use the status indicator to monitor the MPC Controller block in real time. See *Monitoring Optimization Status to Detect Controller Failures* for more details.

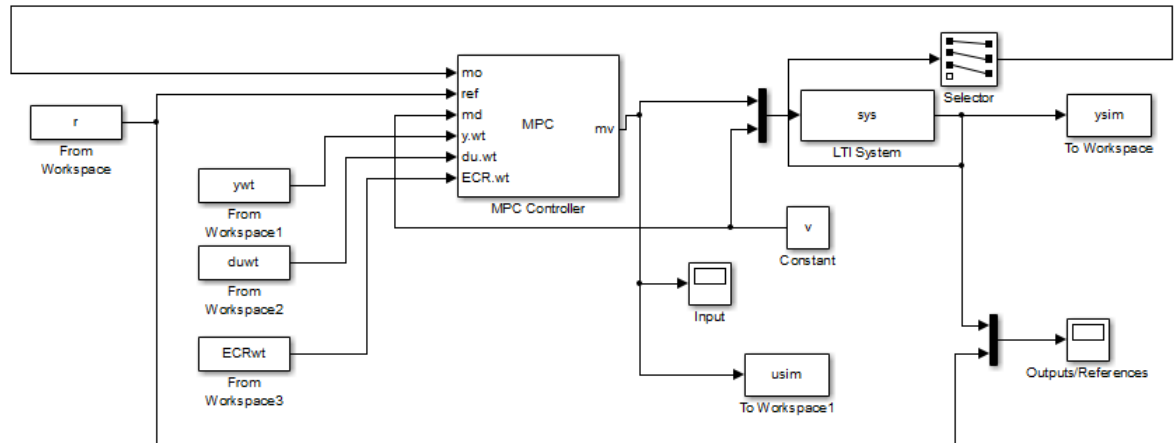


## Online Tuning Inports

A controller intended for real-time applications should have “knobs” you can use to tune its performance when it operates with the real plant. This group of optional inports serves that purpose.

The diagram shown below displays the MPC Controller block’s three tuning knobs. In this simulation context, the knobs are being tuned by prestored signals (the `ywt`, `duwt`, and `ECRwt` variables in the From Workspace blocks). In practice, you would connect a knob or similar manual adjustment.





## Weights on plant outputs

Add an input (`y.wt`) whose input is a vector signal defining a nonnegative weight for each controlled output variable (OV). This signal overrides the `MPCObj.Weights.OV` property, which establishes the relative importance of OV reference tracking.

For example, if the preceding controller defined 3 OVs, the signal connected to the `y.wt` input should be a vector with 3 elements. If the second element is relatively large, the controller would place a relatively high priority on making OV(2) track the `r(2)` reference signal. Setting a `y.wt` signal to zero turns off reference tracking for that OV.

If you do not connect a signal to the `y.wt` input, the block uses the OV weights specified in your MPC object, and these values remain constant.

## Weights on manipulated variables rate

Add an input (`du.wt`), whose input is a vector signal defining  $nu$  nonnegative weights, where  $nu$  is the number of manipulated variables (MVs). The input overrides the `MPCObj.Weights.MVrate` property stored in the mpc object.

For example, if your controller defines four MVs and the second `du.wt` element is relatively large, the controller would use relatively small

# MPC Controller

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changes in the second MV. Such move suppression makes the controller less aggressive. However, too much suppression makes it sluggish.

If you do not connect a signal to the `du.wt` inport, the block uses the `MVrate` weights property specified in your `mpc` object, and these values remain constant.

## **Weight on overall constraint softening**

Add an inport (`ECR.wt`), whose input is a scalar nonnegative signal that overrides the MPC Controller block's `MPCobj.Weights.ECR` property. This inport has no effect unless your controller object defines soft constraints whose associated ECR values are nonzero.

If there are soft constraints, increasing the `ECR.wt` value makes these constraints relatively harder. The controller then places a higher priority on minimizing the magnitude of the predicted worst-case constraint violation.

You may not be able to avoid violations of an output variable constraint. Thus, increasing the `ECR.wt` value is often counterproductive. Such an increase causes the controller to pay less attention to its other objectives and does not help reduce constraint violations. You usually need to tune `ECR.wt` to achieve the proper balance in relation to the other control objectives.

## **Signal Attributes and Block Sample Time**

### **Output data type**

Specify the data type of the manipulated variables (MV) as one of the following:

- `double` — Double-precision floating point (default).
- `single` — Single-precision floating point.

You specify the output data type as `single` if you are implementing the model predictive controller on a single-precision target.

For an example of double- and single-precision simulation and code generation for an MPC controller, see “Simulation and Code Generation Using Simulink Coder”.

To view the port data types in a model, in the Simulink Editor, select **Display > Signals & PortsPort Data Types**. For more information, see “Display Port Data Types”.

### **Block uses inherited sample time (-1)**

Use the sample time inherited from the parent subsystem as the MPC Controller block’s sample time.

Inheriting the sample time allows you to conditionally execute the MPC Controller block inside the Function-Call Subsystem or Triggered Subsystem blocks. For an example, see Using MPC Controller Block Inside Function-Call and Triggered Subsystems.

---

**Note** When you place an MPC controller inside a Function-Call Subsystem or Triggered Subsystem block, you must execute the subsystem at the controller’s design sample rate. You may see unexpected results if you use an alternate sample rate.

---

To view the sample time of a block, in the Simulink Editor, select **Display > Sample Time**. Select **Colors**, **Annotations**, or **All**. For more information, see “View Sample Time Information”.

## **See Also**

`mpc` | `mpcstate` | Multiple MPC Controllers

## **Related Examples**

- MPC Control with Input Quantization Based on Comparing the Optimal Costs
- Analysis of Control Sequences Optimized by MPC on a Double Integrator System
- “Simulation and Code Generation Using Simulink Coder”
- “Simulation and Structured Text Generation Using PLC Coder”

# Multiple MPC Controllers

---

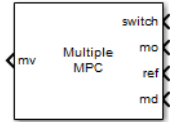
## Purpose

Simulate switching between multiple MPC controllers

## Library

MPC Simulink Library

## Description

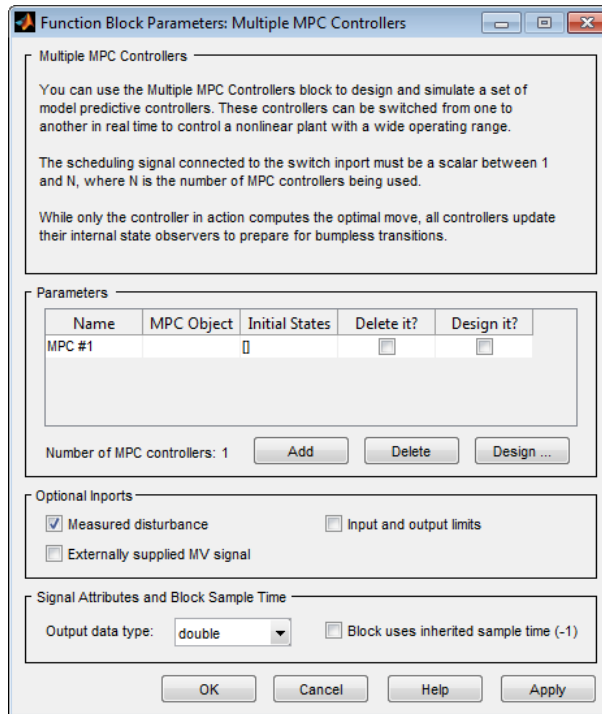


The Multiple MPC Controllers block receives the current measured output, reference signal, and measured disturbance signal. It then solves a quadratic program to calculate the optimal manipulated variables. It also receives a switching signal that designates which one of two or more controllers is to perform the calculation (i.e., the active controller). The block contains these controllers as MPC objects, each of which is designed for a particular operating region of a nonlinear plant.

The Multiple MPC Controllers block allows you to achieve better control of a nonlinear plant over a range of operating conditions. A controller that works well initially can degrade if the plant is nonlinear and its operating point changes. In conventional feedback control, you might compensate for this degradation by gain scheduling. In a similar manner, the Multiple MPC Controllers block allows you to transition between multiple MPC controllers in real time in a preordained manner. You design each controller to work well in a particular region of the operating space. When the plant moves away from this region, you instruct another MPC controller to take over.

The Multiple MPC Controllers block does not provide all the optional features found in the MPC Controller block. The following ports are currently not available:

- Optional outputs such as optimal cost, optimal control sequence, and optimization status
- Optional inports for online tuning



## Dialog Box

The MPC Controller block has the following parameter groupings:

- “Parameters” on page 2-18
- “Required Inports” on page 2-19
- “Required Outports” on page 2-20
- “Optional Inports” on page 2-20
- “Signal Attributes and Block Sample Time” on page 2-24

# Multiple MPC Controllers

---

## Parameters

### MPC Object List

The table is an ordered list of MPC objects. The first row designates the controller to be used when the switch input equals a certain number. The first designates which controller is used when the switch input equals 1, the second when the switch input equals 2, and so on. These controllers must refer to objects that already exist in your base workspace.

---

**Note** After entering each MPC object name, press **Enter**. Also press **Enter** after editing an object name.

---

Use **Add** and **Delete** to add and remove rows. When deleting, indicate any rows to delete using the **Delete It** check box.

When the edit box is empty, and the block is connected to the plant, clicking the **Design** button constructs a default MPC controller. This controller is constructed using a linearized plant model from the Simulink diagram. This action also opens the design tool so you can modify the default behavior.

You can also start the design tool by selecting one or more MPC objects using the **Design It** check box and then clicking **Design**. All selected MPC objects are loaded into the design tool where you can review and edit their properties.

### Initial controller state

Initial state of each MPC object in the ordered list. Each must be a valid `mpcstate` object. If no value is supplied, the default is the nominal value defined in the `Model.Nominal` property of the `mpc` object.

## Required Inports

### Controller Selection

The switch input signal must be a scalar integer between 1 and  $n_c$ , where  $n_c$  is the number of controllers listed in your block mask. At each control instant, this signal designates the controller that will be used.

### Measured output

At each control instant, the `mo` signal must contain the current output variable measurements. Let  $n_{ym}$  be the number of measured output variables (MO) defined in your predictive controller. If  $n_{ym}=1$ , connect a scalar signal to the `mo` inport. Otherwise, connect a row or column vector signal containing  $n_{ym}$  real, double-precision elements.

### Reference

At each control instant, the `ref` signal must contain the current reference values (targets or setpoints) for the  $n_y$  output variables ( $n_y = n_{ym} + \text{number of unmeasured outputs}$ ). You have the option to specify future reference values (previewing).

The `ref` signal must be size  $N$  by  $n_y$ , where  $N(1 \leq N \leq p)$  is the number of time steps for which you are specifying reference values and  $p$  is the prediction horizon. Each element must be a real, double-precision number. The `ref` dimension must not change from one control instant to the next.

When  $N=1$ , you cannot preview. To specify future reference values, choose  $N$  such that  $1 < N \leq p$  to enable previewing. Doing so usually improves performance via `feedforward` information. The first row specifies the  $n_y$  references for the first step in the prediction horizon (at the next control interval  $k=1$ ), and so on for  $N$  steps. If  $N < p$ , the last row designates constant reference values to be used for the remaining  $p-N$  steps.

# Multiple MPC Controllers

---

For example, suppose  $n_y=2$  and  $p=6$ . At a given control instant, the signal connected to the controller's ref inport is

```
[ 2 5   k=1
  2 6   k=2
  2 7   k=3
  2 8]  k=4
```

The signal informs the controller that:

- Reference values for the first prediction horizon step ( $k=1$ ) are 2 and 5.
- The first reference value remains at 2, but the second increases gradually.
- The second reference value becomes 8 at the beginning of the fourth step ( $k=4$ ) in the prediction horizon.
- Both values remain constant at 2 and 8 respectively for steps 5–6 of the prediction horizon.

## Required Outputs

### Manipulated Variables

The mv output provides a signal defining the  $n_u \geq 1$  manipulated variables, which are to be implemented in the plant. The controller updates its mv output by solving a quadratic program at each control instant. The elements are real, double-precision values.

### Optional Inports

#### Measured disturbance

Add an inport (md) to which you can connect a measured disturbance signal.

Your measured disturbance signal (MD) must be size  $N \times n_{md}$ , where  $n_{md}(\geq 1)$  is the number of measured disturbances defined in your Model Predictive Controller and  $N$  ( $1 \leq N \leq p+1$ ) is the number of time steps for which the MD is known. Each element must be a real,



double-precision number. The signal dimensions must not change from one control instant to the next.

If  $N=1$  you cannot preview. At each control instant, the MD signal must contain the most recent measurements at the current time  $k=0$  (as a row vector, length  $n_{md}$ ). The controller assumes that the MDs remain constant at their current values for the entire prediction horizon.

If you are able to predict future MD values, choose  $N$  such that  $1 < N \leq p+1$  to enable previewing. Doing so usually improves performance via **feedforward**. In this case, the first row must contain the  $n_{md}$  current values at  $k=0$ , and the remaining rows designate variations over the next  $N-1$  control instants. If  $N < p+1$ , the last row designates constant MD values to be used for the remaining  $p+1-N$  steps of the prediction horizon.

For example suppose  $n_{md}=2$  and  $p=6$ . At a given control instant, the signal connected to the controller's md inport is:

```
[2 5      k=0
 2 6      k=1
 2 7      k=2
 2 8]     k=3
```

This signal informs the controller that:

- The current MDs are 2 and 5 at  $k=0$ .
- The first MD remains at 2, but the second increases gradually.
- The second MD becomes 8 at the beginning of the step 3 ( $k=3$ ) in the prediction horizon.
- Both values remain constant at 2 and 8 respectively for steps 4–6 of the prediction horizon.

`mpcpreview` shows how to use MD previewing in a specific case.

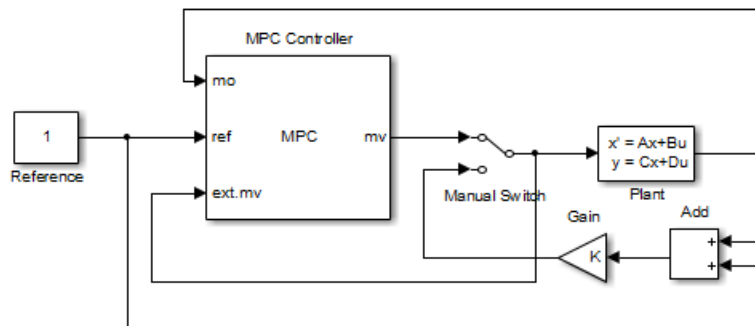
For calculation details, see “Prediction Model” and “QP Matrices”.

# Multiple MPC Controllers

## Externally supplied MV signals

Add an inport (`ext.mv`), which you can connect to the actual manipulated variables (MV) used in the plant. The block uses these to update its internal state estimates. For example, suppose the actual signals saturate at physical limits or the MV is under manual control. In both cases, feeding the actual value back to the MPC Controller block can improve performance significantly, because the prediction model's state estimates are updated more accurately.

The following example shows how a manual switch may override the controller's output. Also see [Turning Controller Online and Offline with Bumpless Transfer](#).



Do not connect this option to leave the `ext.mv` inport unconnected. In either case, the model predictive controller assumes that the plant uses the MV signals sent by the MPC Controller block. In the preceding example, the external MV signal always provides the model predictive controller that the control signal actually used in the plant. Otherwise, the model predictive controller's internal state estimate would be inaccurate.

---

**Note** The MPC Controller block is a discrete-time block with sampling time inherited from the MPC object. The MPC block has direct feedthrough from measured outputs (`mo`), output references (`ref`), and measured disturbances (`md`) to MPC-manipulated variables (`mv`). There is no direct feedthrough from externally supplied manipulated variables (`ext.mv`) to MPC-manipulated variables (`mv`).

---

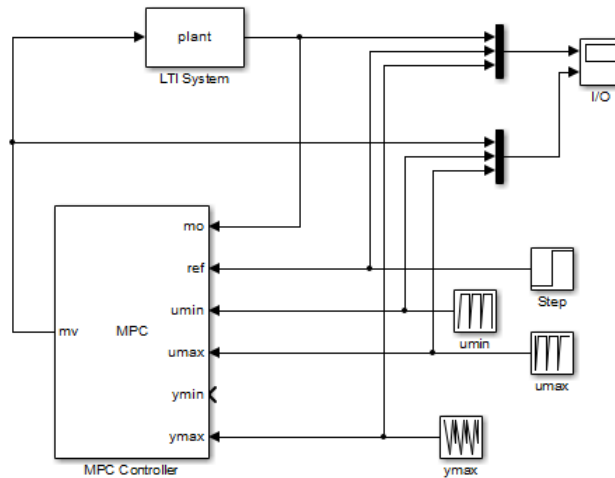
### Input and output limits

Add inports (`umin,umax,ymin,ymax`), which you can connect to run-time constraint signals. If this check box is not selected, the block uses the constant constraint values stored within its `mpc` object. Example connections appear in the following model. See Varying Input and Output Constraints for an example of using this option.

Each unconnected limit inport, such as `ymin` in the following model, is treated as an unbounded signal. The corresponding constraint settings in the `mpc` object must also be unbounded. For connected limit inports, such as `ymax`, the signals must be finite and the corresponding variables in the `mpc` object must also be bounded.

All constraint signals connected to the block must be finite. Also, you cannot change the number or identity of constrained and unconstrained variables. For example, if your `mpc` object specifies that your first MV has a lower bound, you must supply a `umin` signal for it.

# Multiple MPC Controllers



## Signal Attributes and Block Sample Time

### Output data type

Specify the data type of the manipulated variables (MV) as one of the following:

- `double` — Double-precision floating point (default).
- `single` — Single-precision floating point.

You specify the output data type as `single` if you are implementing the model predictive controller on a single-precision target.

For an example of double- and single-precision simulation and code generation for an MPC controller, see “Simulation and Code Generation Using Simulink Coder”.

To view the port data types in a model, in the Simulink Editor, select **Display > Signals & PortsPort Data Types**. For more information, see “Display Port Data Types”.

## **Block uses inherited sample time (-1)**

Use the sample time inherited from the parent subsystem as the Multiple MPC Controllers block's sample time.

Inheriting the sample time allows you to conditionally execute the Multiple MPC Controllers block inside the Function-Call Subsystem or Triggered Subsystem blocks. For an example, see [Using MPC Controller Block Inside Function-Call and Triggered Subsystems](#).

---

**Note** When you place an MPC controller inside a Function-Call Subsystem or Triggered Subsystem block, you must execute the subsystem at the controller's design sample rate. You may see unexpected results if you use an alternate sample rate.

---

To view the sample time of a block, in the Simulink model window, select **Display > Sample Time**. Select **Colors**, **Annotations**, or **All**. For more information, see "View Sample Time Information".

## **See Also**

[mpc](#) | [mpcmove](#) | [mpcstate](#) | [MPC Controller](#)

## **Related Examples**

- [Scheduling Controllers for a Plant with Multiple Operating Points](#)
- [Chemical Reactor with Multiple Operating Points](#)
- ["Simulation and Code Generation Using Simulink Coder"](#)
- ["Simulation and Structured Text Generation Using PLC Coder"](#)

# Multiple MPC Controllers

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# Object Reference

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- “MPC Controller Object” on page 3-2
- “MPC Simulation Options Object” on page 3-14
- “MPC State Object” on page 3-16

## MPC Controller Object

All the parameters defining the MPC control law (prediction horizon, weights, constraints, etc.) are stored in an MPC object, whose properties are listed in the following table (MPC Controller Object on page 3-2).

### MPC Controller Object

Property	Description
ManipulatedVariables (or MV or Manipulated or Input )	Input and input-rate upper and lower bounds, ECR values, names, units, and input target
OutputVariables (or OV or Controlled or Output )	Output upper and lower bounds, ECR values, names, units
DisturbanceVariables (or DV or Disturbance )	Disturbance names and units
Weights	Weights defining the performance function
Model	Plant, input disturbance, and output noise models, and nominal conditions.
Ts	Controller's sampling time
Optimizer	Parameters for the QP solver
PredictionHorizon	Prediction horizon
ControlHorizon	Number of free control moves or vector of blocking moves
History	Creation time
Notes	Text or comments about the MPC controller object
UserData	Any additional data



**MPC Controller Object (Continued)**

Property	Description
MPCData (private)	Matrices for the QP problem and other accessorial data
Version (private)	Model Predictive Control Toolbox version number

**ManipulatedVariables**

**ManipulatedVariables** (or MV or Manipulated or Input) is an  $n_u$ -dimensional array of structures ( $n_u$  = number of manipulated variables), one per manipulated variable. Each structure has the fields described in the following table (Structure ManipulatedVariables on page 3-3), where  $p$  denotes the prediction horizon.

**Structure ManipulatedVariables**

Field Name	Content	Default
Min	1 to $p$ dimensional vector of lower constraints on a manipulated variable $u$	-Inf
Max	1 to $p$ dimensional vector of upper constraints on a manipulated variable $u$	Inf
MinECR	1 to $p$ dimensional vector describing the equal concern for the relaxation of the lower constraints on $u$	0
MaxECR	1 to $p$ dimensional vector describing the equal concern for the relaxation of the upper constraints on $u$	0
Target	1 to $p$ dimensional vector of target values for the input variable $u$	'nominal'

**Structure ManipulatedVariables (Continued)**

Field Name	Content	Default
RateMin	1 to $p$ dimensional vector of lower constraints on the rate of a manipulated variable $u$	-Inf if problem is unconstrained, otherwise -10
RateMax	1 to $p$ dimensional vector of upper constraints on the rate of a manipulated variable $u$	Inf
RateMinECR	1 to $p$ dimensional vector describing the equal concern for the relaxation of the lower constraints on the rate of $u$	0
RateMaxECR	1 to $p$ dimensional vector describing the equal concern for the relaxation of the upper constraints on the rate of $u$	0
Name	Name of input signal. This is inherited from InputName of the LTI plant model.	InputName of LTI plant model
Units	String specifying the measurement units for the manipulated variable	' '

---

**Note** Rates refer to the difference  $\Delta u(k)=u(k)-u(k-1)$ . Constraints and weights based on derivatives  $du/dt$  of continuous-time input signals must be properly reformulated for the discrete-time difference  $\Delta u(k)$ , using the approximation  $du/dt \cong \Delta u(k)/T_s$ .

---

**OutputVariables**

OutputVariables (or OV or Controlled or Output) is an  $n_y$ -dimensional array of structures ( $n_y$  = number of outputs), one per output signal. Each structure has the fields described in the following table (Structure OutputVariables on page 3-5), where  $p$  denotes the prediction horizon.

### Structure OutputVariables

Field Name	Content	Default
Min	1 to $p$ dimensional vector of lower constraints on an output $y$	- Inf
Max	1 to $p$ dimensional vector of upper constraints on an output $y$	Inf
MinECR	1 to $p$ dimensional vector describing the equal concern for the relaxation of the lower constraints on an output $y$	1
MaxECR	1 to $p$ dimensional vector describing the equal concern for the relaxation of the upper constraints on an output $y$	1
Name	Name of output signal. This is inherited from OutputName of the LTI plant model.	OutputName of LTI plant model
Units	String specifying the measurement units for the measured output	' '
Integrator	Magnitude of integrated white noise on the output channel (0=no integrator)	[ ]

In order to reject constant disturbances due for instance to gain nonlinearities, the default output disturbance model used in Model Predictive Control Toolbox software is a collection of integrators driven by white noise on measured outputs (see “Output Disturbance Model” in the Model Predictive Control Toolbox User’s Guide). Output integrators are added according to the following rule:

- 1 Measured outputs are ordered by decreasing output weight (in case of time-varying weights, the sum of the absolute values over time is considered for each output channel, and in case of equal output weight, the order within the output vector is followed).

- 2 By following such order, an output integrator is added per measured outputs, unless there is a violation of observability, or you force it by zeroing the corresponding value in `OutputVariables.Integrators`.

By default, `OutputVariables.Integrators` is empty on all outputs. This enforces the default action of Model Predictive Control Toolbox software, namely add integrators on measured outputs, do not add integrators on unmeasured outputs. By setting the entry of `OutputVariables(i).Integrators` to zero, no attempt will be made to add integrated white noise on the *i*-th output. On the contrary, by setting the entry of `OutputVariables(i).Integrators` to one, an attempt will be made to add integrated white noise on the *i*-th output (see `getoutdist`).

## DisturbanceVariables

`DisturbanceVariables` (or DV or Disturbance) is an  $(n_v+n_d)$ -dimensional array of structures ( $n_v$  = number of measured input disturbances,  $n_d$  = number of unmeasured input disturbances), one per input disturbance. Each structure has the fields described in the following table (Structure `DisturbanceVariables` on page 3-6).

### Structure `DisturbanceVariables`

Field Name	Content	Default
Name	Name of input signal. This is inherited from <code>InputName</code> of the LTI plant model.	<code>InputName</code> of LTI plant model
Units	String specifying the measurement units for the manipulated variable	''

The order of the disturbance signals within the array `DisturbanceVariables` is the following: the first  $n_v$  entries relate to measured input disturbances, the last  $n_d$  entries relate to unmeasured input disturbances.

---

**Note** The Name properties of `ManipulatedVariables`, `OutputVariables`, and `DisturbanceVariables` are read only. You can set signal names in the `Model.Plant.InputName` and `Model.Plant.OutputName` properties of the MPC object, for instance by using the method `setname`.

---

## Weights

`Weights` is the structure defining the QP weighting matrices. Unlike the `InputSpecs` and `OutputSpecs`, which are arrays of structures, `weights` is a single structure containing four fields. The values of these fields depend on whether you are using the standard quadratic cost function (see “Standard Form”) or the alternative cost function (see “Alternative Cost Function”).

### Standard Cost Function

The table below, `Weights` for the Standard Cost Function (MATLAB® Structure) on page 3-7, lists the content of the four fields where  $p$  denotes the prediction horizon,  $n_u$  the number of manipulated variables,  $n_y$  the number of output variables.

The fields `ManipulatedVariables`, `ManipulatedVariablesRate`, and `OutputVariables` are arrays with  $n_u$ ,  $n_u$ , and  $n_y$  columns, respectively. If weights are time invariant, then `ManipulatedVariables`, `ManipulatedVariablesRate`, and `OutputVariables` are row vectors. However, for time-varying weights, each field is a matrix with up to  $p$  rows. If the number of rows is less than the prediction horizon,  $p$ , the object constructor duplicates the last row to create a matrix with  $p$  rows.

### Weights for the Standard Cost Function (MATLAB Structure)

Field Name	Content	Default
<code>ManipulatedVariables</code> (or <code>MV</code> or <code>Manipulated</code> or <code>Input</code> )	(1 to $p$ )-by- $n_u$ dimensional array of input weights	<code>zeros(1,nu)</code>
<code>ManipulatedVariablesRate</code> (or <code>MVRate</code> or <code>ManipulatedRate</code> or <code>InputRate</code> )	(1 to $p$ )-by- $n_u$ dimensional array of input-rate weights	<code>0.1*ones(1,nu)</code>

**Weights for the Standard Cost Function (MATLAB Structure) (Continued)**

Field Name	Content	Default
OutputVariables (or OV or Controlled or Output)	(1 to $p$ )-by- $n_y$ dimensional array of output weights	1 (The default for output weights is the following: if $n_u \geq n_y$ , all outputs are weighted with unit weight; if $n_u < n_y$ , $n_u$ outputs are weighted with unit weight (with preference given to measured outputs), while the remaining outputs receive zero weight.)
ECR	Weight on the slack variable $\epsilon$ used for softening the constraints	$1e5 * (\text{max weight})$

The default ECR weight is  $10^5$  times the largest weight specified in ManipulatedVariables, ManipulatedVariablesRate, and OutputVariables.

---

**Note** All weights must be greater than or equal to zero. If all weights on manipulated variable increments are strictly positive, the resulting QP problem is always strictly convex. If some of those weights are zero, the Hessian matrix of the QP problem may become only positive semidefinite. In order to keep the QP problem always strictly convex, if the condition number of the Hessian matrix  $K_{\Delta U}$  is larger than  $10^{12}$ , the quantity  $10 * \text{sqrt}(\text{eps})$  is added on each diagonal term. This may only occur when all input rates are not weighted ( $W^{\Delta u} = 0$ ) (see “Cost Function” in the *Model Predictive Control Toolbox User’s Guide*).

---

**Alternative Cost Function**

You can specify off-diagonal Q and R weight matrices in the cost function. To accomplish this, you must define the fields ManipulatedVariables, ManipulatedVariablesRate, and OutputVariables as cell arrays, each containing a single positive-semi-definite matrix of the appropriate size. Specifically, OutputVariables must be a cell array containing the  $n_y$ -by- $n_y$

$Q$  matrix, `ManipulatedVariables` must be a cell array containing the  $n_u$ -by- $n_u$   $R_u$  matrix, and `ManipulatedVariablesRate` must be a cell array containing the  $n_u$ -by- $n_u$   $R_{\Delta u}$  matrix (see “Alternative Cost Function”) and the `mpcweightdemo` example). You can abbreviate the field names as shown in `Weights for the Standard Cost Function (MATLAB® Structure)` on page 3-7. You can also use diagonal weights (as defined in `Weights for the Standard Cost Function (MATLAB® Structure)` on page 3-7) for one or more of these fields. If you omit a field, the object constructor uses the defaults shown in `Weights for the Standard Cost Function (MATLAB® Structure)` on page 3-7.

For example, you can specify off-diagonal weights, as follows

```
MPCobj.Weights.OutputVariables={Q};
MPCobj.ManipulatedVariables={Ru};
MPCobj.ManipulatedVariablesRate={Rdu};
```

where  $Q=Q$ ,  $Ru=R_u$ , and  $Rdu = R_{\Delta u}$  are positive semidefinite matrices.

---

**Note** You cannot specify off-diagonal time-varying weights.

---

## Model

The property `Model` specifies plant, input disturbance, and output noise models, and nominal conditions, according to the model setup described in “State Estimation”. It is specified through a structure containing the fields reported in `Structure Model Describing the Models Used by MPC` on page 3-9.

### Structure Model Describing the Models Used by MPC

Field Name	Content	Default
Plant	LTI model or identified linear model of the plant	No default
Disturbance	LTI model describing color of input disturbances	An integrator on each Unmeasured input channel

### Structure Model Describing the Models Used by MPC (Continued)

Field Name	Content	Default
Noise	LTI model describing color of plant output measurement noise	Unit white noise on each measured output = identity static gain
Nominal	Structure containing the state, input, and output values where <code>Model.Plant</code> is linearized	See Nominal Values at Operating Point on page 3-11.

---

**Note** Direct feedthrough from manipulated variables to any output in `Model.Plant` is not allowed. See “Prediction Model” in the Model Predictive Control Toolbox User’s Guide.

---

The type of input and output signals is assigned either through the `InputGroup` and `OutputGroup` properties of `Model.Plant`, or, more conveniently, through function `setmpcsignals`, according to the nomenclature described in Input Groups in Plant Model on page 3-10 and Output Groups in Plant Model on page 3-11.

#### Input Groups in Plant Model

Name	Value
ManipulatedVariables (or MV or Manipulated or Input)	Indices of manipulated variables
MeasuredDisturbances (or MD or Measured)	Indices of measured disturbances
UnmeasuredDisturbances (or UD or Unmeasured)	Indices of unmeasured disturbances



## Output Groups in Plant Model

Name	Value
MeasuredOutputs (or MO or Measured)	Indices of measured outputs
UnmeasuredOutputs (or UO or Unmeasured)	Indices of unmeasured outputs

By default, all inputs are manipulated variables, and all outputs are measured.

---

**Note** With this current release, the `InputGroup` and `OutputGroup` properties of LTI objects are defined as structures, rather than cell arrays (see the Control System Toolbox documentation for more details).

---

The structure `Nominal` contains the nominal values for states, inputs, outputs and state derivatives/differences at the operating point where `Model.Plant` was linearized. The fields are reported in Nominal Values at Operating Point on page 3-11 (see “Offsets” in the Model Predictive Control Toolbox User’s Guide).

## Nominal Values at Operating Point

Field	Description	Default
X	Plant state at operating point	0
U	Plant input at operating point, including manipulated variables, measured and unmeasured disturbances	0
Y	Plant output at operating point	0
DX	For continuous-time models, DX is the state derivative at operating point: $DX=f(X,U)$ . For discrete-time models, $DX=x(k+1)-x(k)=f(X,U)-X$ .	0

## Ts

Sampling time of the MPC controller. By default, if `Model.Plant` is a discrete-time model, `Ts=Model.Plant.ts`. For continuous-time plant models, you must specify a sampling time for the MPC controller.

## Optimizer

Parameters for the QP optimization. `Optimizer` is a structure with the fields reported in the following table (Optimizer Properties on page 3-12).

### Optimizer Properties

Field	Description	Default
<code>MaxIter</code>	Maximum number of iterations allowed in the QP solver	200
<code>Trace</code>	On/off	'off'
<code>Solver</code>	QP solver used (only 'ActiveSet')	'ActiveSet'
<code>MinOutputECR</code>	Minimum positive value allowed for <code>OutputMinECR</code> and <code>OutputMaxECR</code>	1e-10

`MinOutputECR` is a positive scalar used to specify the minimum allowed ECR for output constraints. If values smaller than `MinOutputECR` are provided in the `OutputVariables` property of the MPC objects a warning message is issued and the value is raised to `MinOutputECR`.

## PredictionHorizon

`PredictionHorizon` is an integer value expressing the number  $p$  of sampling steps of prediction.

## ControlHorizon

`ControlHorizon` is either a number of free control moves, or a vector of blocking moves (see “Optimization Variables” in the Model Predictive Control Toolbox User’s Guide).

## History

`History` stores the time the MPC controller was created.

## Notes

`Notes` stores text or comments as a cell array of strings.

## UserData

Any additional data stored within the MPC controller object.

## MPCData

`MPCData` is a private property of the MPC object used for storing intermediate operations, QP matrices, internal flags, etc.

## Version

`Version` is a private property indicating the Model Predictive Control Toolbox version number.

## Construction and Initialization

An MPC object is built in two steps. The first step happens *at construction* of the object when the object constructor `mpc` is invoked, or properties are changed by a `set` command. At this first stage, only basic consistency checks are performed, such as dimensions of signals, weights, constraints, etc. The second step happens *at initialization* of the object, namely when the object is used for the first time by methods such as `mpcmove` and `sim`, that require the full computation of the QP matrices and the estimator gain. At this second stage, further checks are performed, such as a test of observability of the overall extended model.

Informative messages are displayed in the command window in both phases, you can turn them on or off using the `mpcverbosity` command.

## MPC Simulation Options Object

The `mpcsimopt` object type contains various simulation options for simulating an MPC controller with the command `sim`. Its properties are listed in the following table (MPC Simulation Options Properties on page 3-14).

### MPC Simulation Options Properties

Property	Description
<code>PlantInitialState</code>	Initial state vector of the plant model generating the data.
<code>ControllerInitialState</code>	Initial condition of the MPC controller. This must be a valid <code>@mpcstate</code> object.
<code>UnmeasuredDisturbance</code>	Unmeasured disturbance signal entering the plant.
<code>InputNoise</code>	Noise on manipulated variables.
<code>OutputNoise</code>	Noise on measured outputs.
<code>RefLookAhead</code>	Preview on reference signal ('on' or 'off').
<code>MDLookAhead</code>	Preview on measured disturbance signal ('on' or 'off').
<code>Constraints</code>	Use MPC constraints ('on' or 'off').
<code>Model</code>	Model used in simulation for generating the data.
<code>StatusBar</code>	Display the wait bar ('on' or 'off').
<code>MVSignal</code>	Sequence of manipulated variables (with offsets) for open-loop simulation (no MPC action).
<code>OpenLoop</code>	Perform open-loop simulation.

The command

```
SimOptions=mpcsimopt(mpcobj)
```

returns an empty @mpcsimopt object. You must use `set / get` to change simulation options.

`UnmeasuredDisturbance` is an array with as many columns as unmeasured disturbances, `InputNoise` and `MVSignal` are arrays with as many columns as manipulated variables, `OutputNoise` is an array with as many columns as measured outputs. The last sample of the array is extended constantly over the horizon to obtain the correct size.

---

**Note** Nonzero values of `ControllerInitialState.LastMove` are only meaningful if there are constraints on the increments of the manipulated variables.

---

The property `Model` is useful for simulating the MPC controller under model mismatch. The LTI object specified in `Model` can be either a replacement for `Model.Plant`, or a structure with fields `Plant`, `Nominal`. By default, `Model` is equal to `MPCobj.Model` (no model mismatch). If `Model` is specified, then `PlantInitialState` refers to the initial state of `Model.Plant` and is defaulted to `Model.Nominal.x`.

If `Model.Nominal` is empty, `Model.Nominal.U` and `Model.Nominal.Y` are inherited from `MPCobj.Model.Nominal`. `Model.Nominal.X/DX` is only inherited if both plants are state-space objects with the same state dimension.

## MPC State Object

The `mpcstate` object type contains the state of an MPC controller. Its properties are listed in MPC State Object Properties on page 3-16.

### MPC State Object Properties

Property	Description
Plant	Array of plant states. Values are absolute, i.e., they include possible state offsets (cf. <code>Model.Nominal.X</code> ).
Disturbance	Array of states of unmeasured disturbance models. This contains the states of the input disturbance model and, appended below, the states of the unmeasured output disturbances model.
Noise	Array of states of measurement noise model.
LastInput	Array of previous manipulated variables $u(k-1)$ . Values are absolute, i.e., they include possible input offsets (cf. <code>Model.Nominal.U</code> ).

The command

```
mpcstate(mpcobj)
```

returns a zero extended initial state compatible with the MPC object `mpcobj`, and with `mpcobj.Plant` and `mpcobj.LastInput` initialized at the nominal values specified in `mpcobj.Model.Nominal`.